

Solar Hydrogen Production

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Introduction

- Motivation: Political, Economical, Ecological, Technical
- Concentrating Solar Systems
- Solar fuels technology developments and demonstrations
- R&D needs and networks

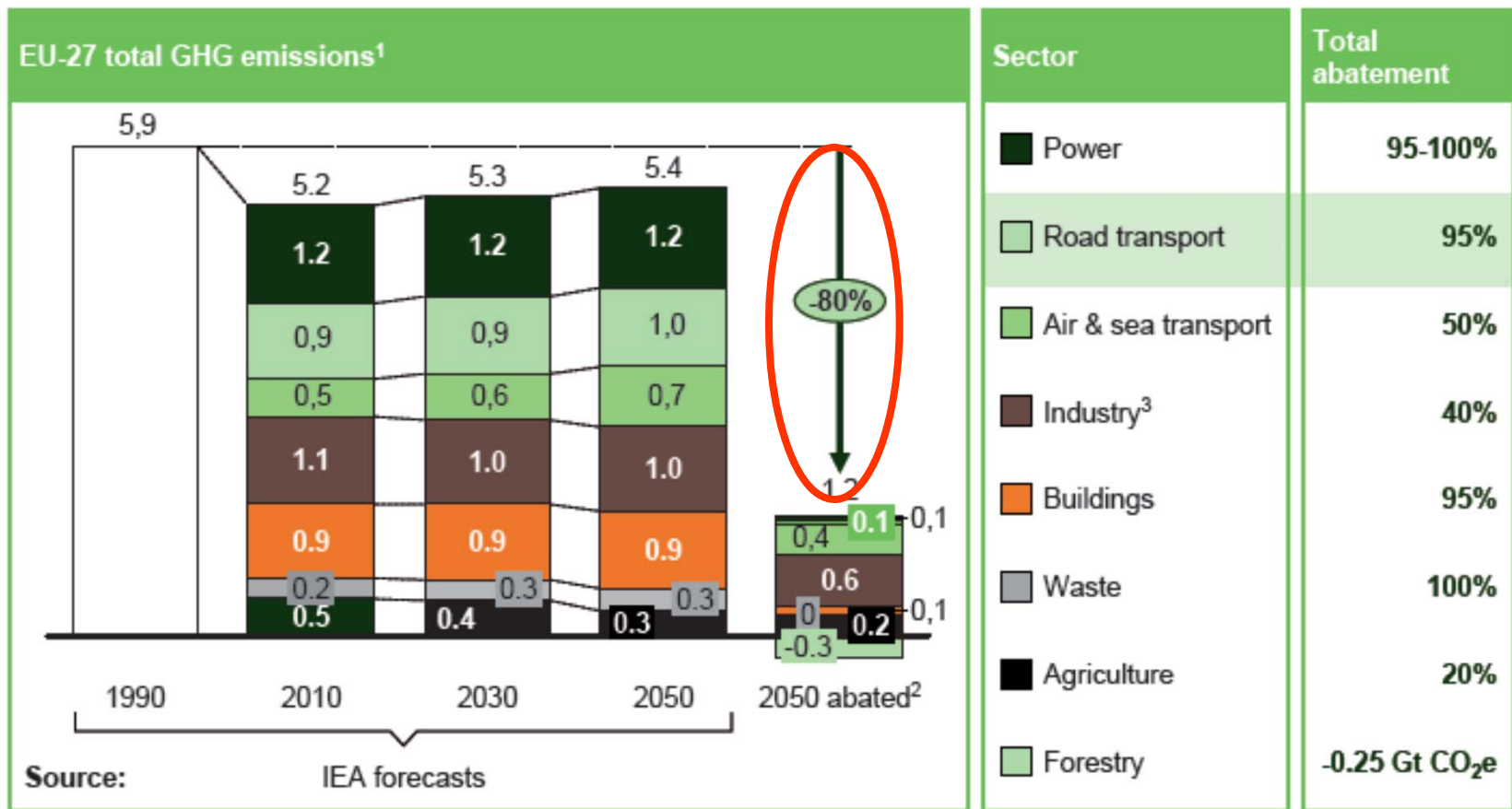


Political Driver: Example – EU Sustainable Energy Technology Plan (SET-Plan 2007)

- **Goals of the EU until 2020 (20/20/20)**
 - **20%** higher energy efficiency
 - **20%** less GHG emission
 - **20%** renewable energy
- **Goal of the EU until 2050:**
 - **80%** less CO₂ emissions than in 1990
- Significant research effort for the development of a new generation of CO₂ emission free energy technologies, like
 - Offshore-Wind
 - **Solar**
 - 2nd generation Biomass



Development of EU GHG emissions [Gt CO₂e]



1 Large efficiency improvements are already included in the baseline based on the International Energy Agency, World Energy Outlook 2009, especially for industry

2 Abatement estimates within sector based on Global GHG Cost Curve

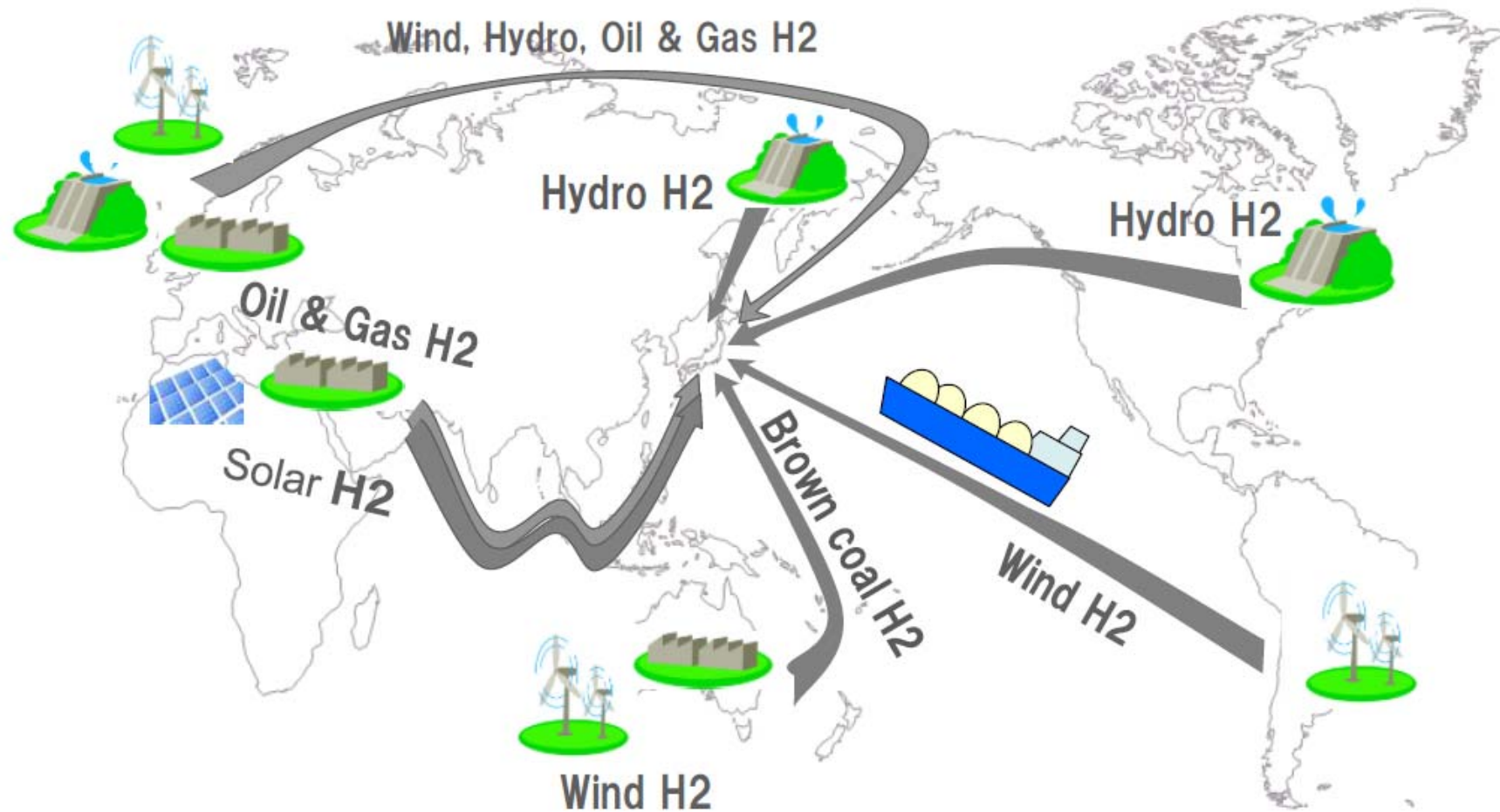
3 CCS applied to 50% of large industry (cement, chemistry, iron and steel, petroleum and gas, not applied to other industries)



SOURCE: www.roadmap2050.eu

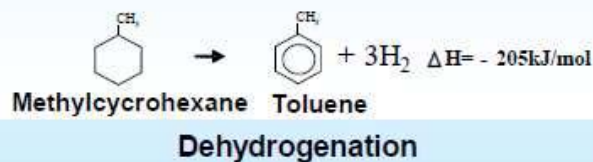
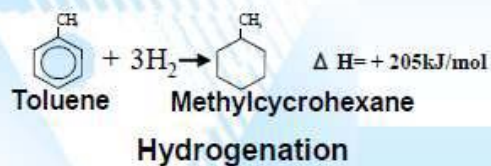
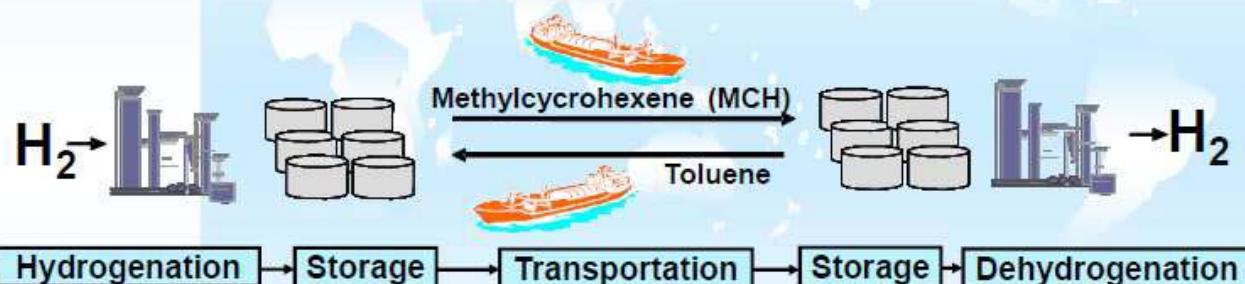


Kawasaki Vision – Hydrogen Potential from Overseas



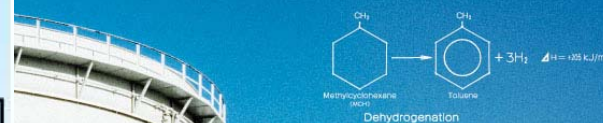
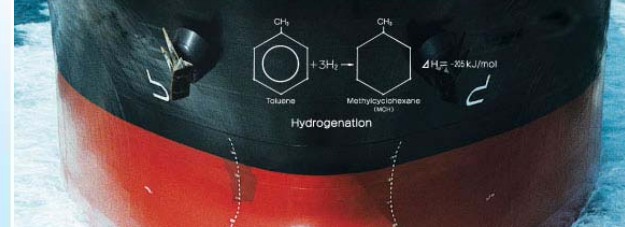
CHIYODA – Hydrogen Vision

The Methylcyclohexene(MCH) is considered one of the safety and economical hydrogen carriers because of the storage and transportation in the liquid phase under the ambient temperature and pressure.



Two technologies defied conventional wisdom and made SPERA Hydrogen possible.

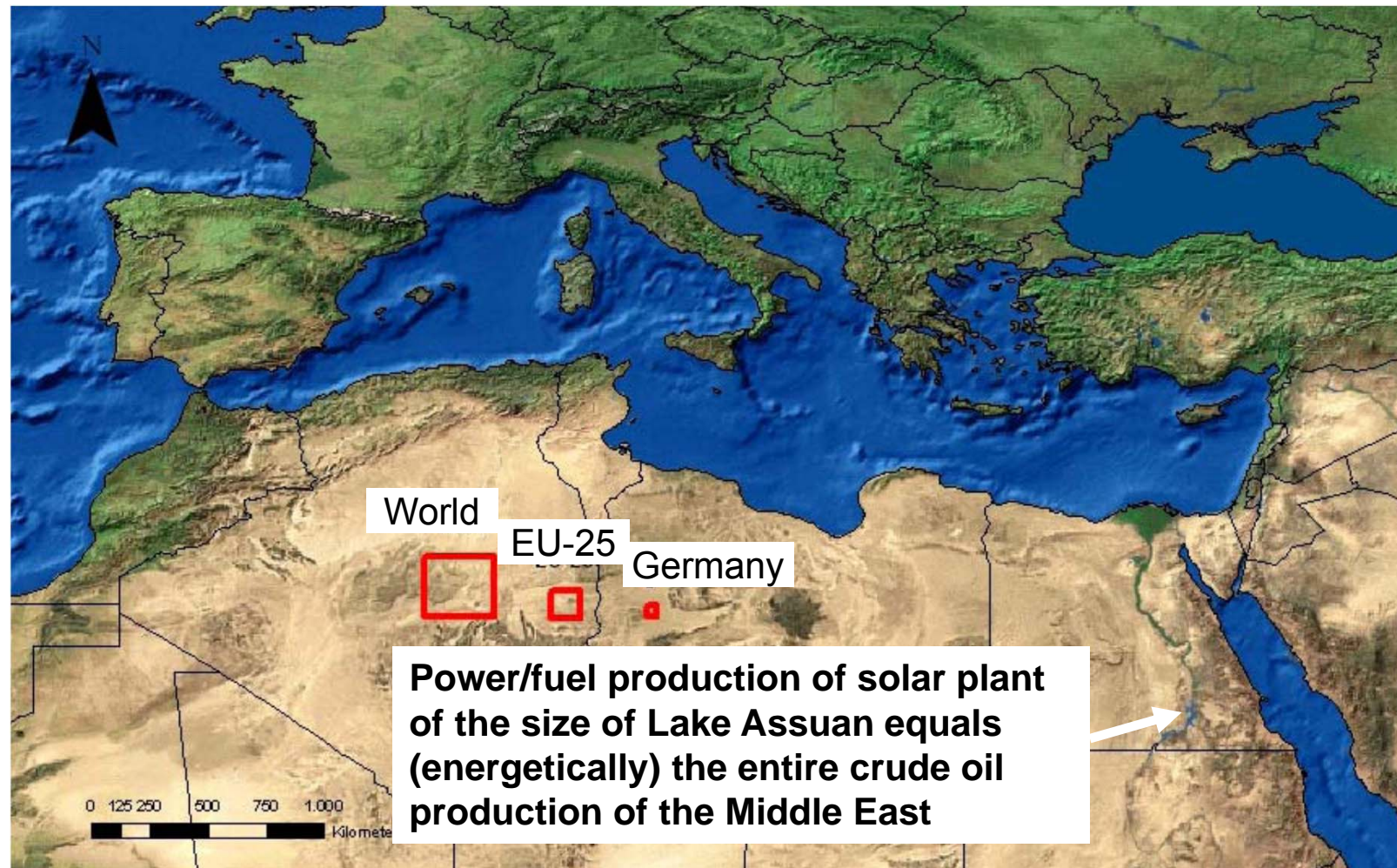
1 ~Organic Chemical Hydride (OCH) Technology~
 Enables the transport of hydrogen at ambient temperature and pressure.
 Fixing hydrogen to toluene, a major component of gasoline, produces a liquid called methylcyclohexane (MCH), which is easy to handle at ambient temperature and pressure. This is SPERA Hydrogen. Our technology facilitates storage of hydrogen in large quantities and long-distance transportation at a low cost because it eliminates the need for hydrogen (the lightest gas, difficult to store or transport under normal conditions) to be liquefied at cryogenic temperatures or pressurized in cylinders.



2 ~Dehydrogenation Catalyst~
 Extracts hydrogen from MCH.
 For some time, the extraction of hydrogen from methylcyclohexane (MCH) had been considered impossible. However Chiyoda Corporation developed a catalyst to achieve exactly that, by means of our proprietary nanotechnology. The catalyst makes it possible to supply just the right amount of hydrogen on demand at any time and any place.



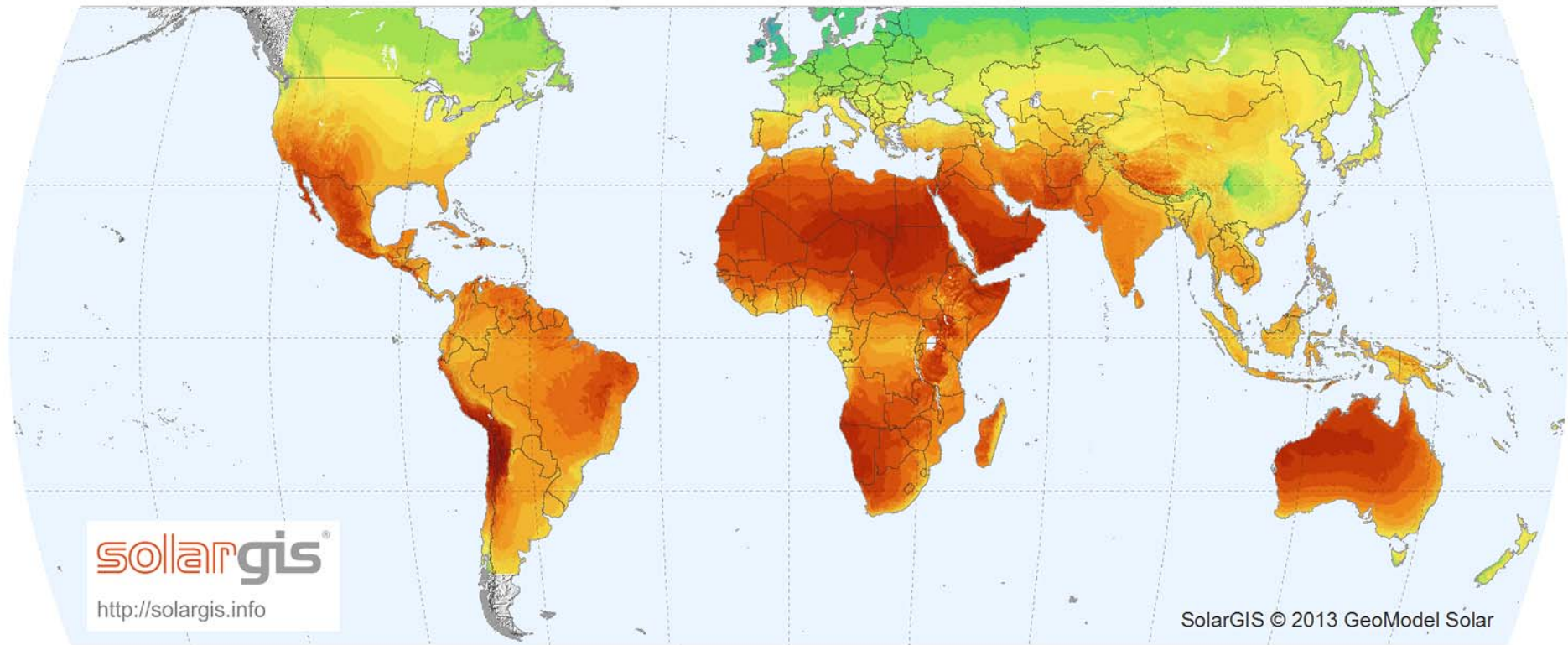
Potential of Solar Energy



Potential of Solar Energy

WORLD MAP OF GLOBAL HORIZONTAL IRRADIATION

GeoModel
SOLAR



Long-term average of: Annual sum < 700 900 1100 1300 1500 1700 1900 2100 2300 2500 2700 >
Daily sum < 2.0 2.5 3.0 3.5 4.0 4.5 5.0 5.5 6.0 6.5 7.0 7.5 > kWh/m²

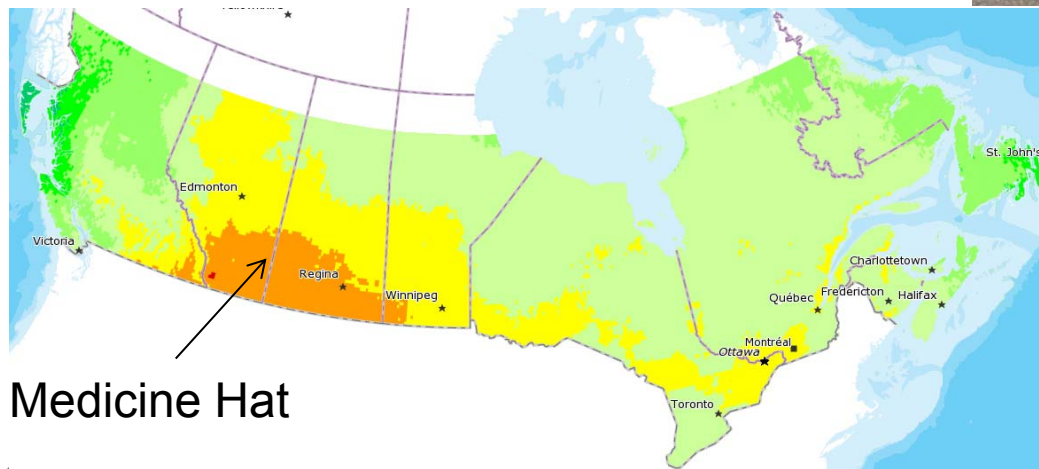


CSP in Canada

1 MW_e Demonstration Plant

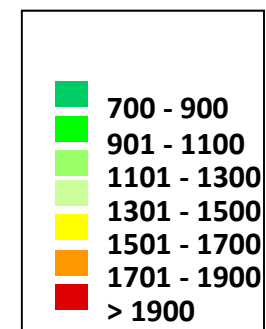
Medicine Hat, Alberta

- Integrated Solar Combined Cycle demonstration with a capacity of 1 MW_e
- Connected to the 203 MW_e municipal power plant
- Location: 50.04° N; 110.72° W
- Average annual DNI 1833 kWh/m²
- Annual output 4100 MWh_{th}



Medicine Hat

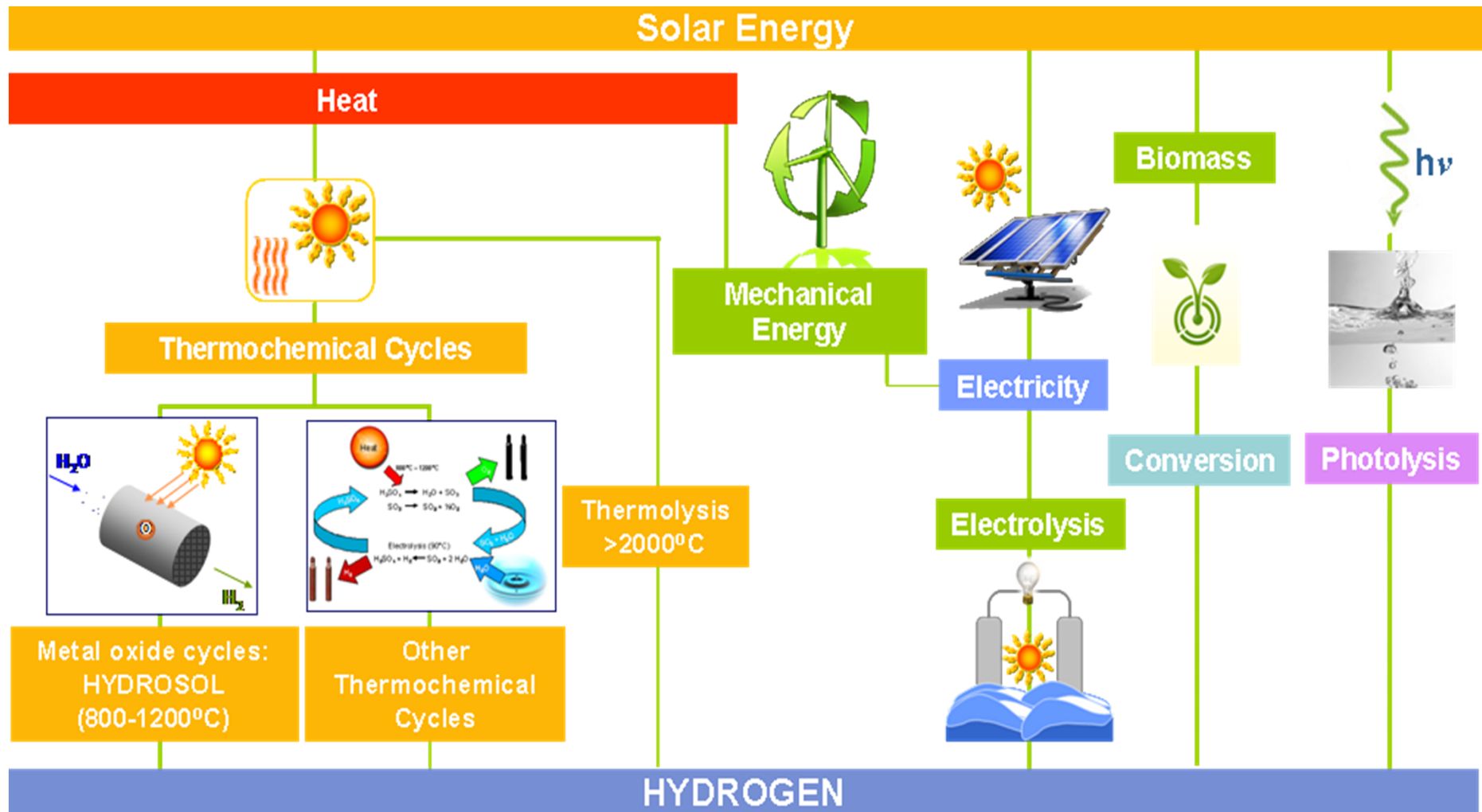
DNI annual average



Source: NRCAN/CANMET



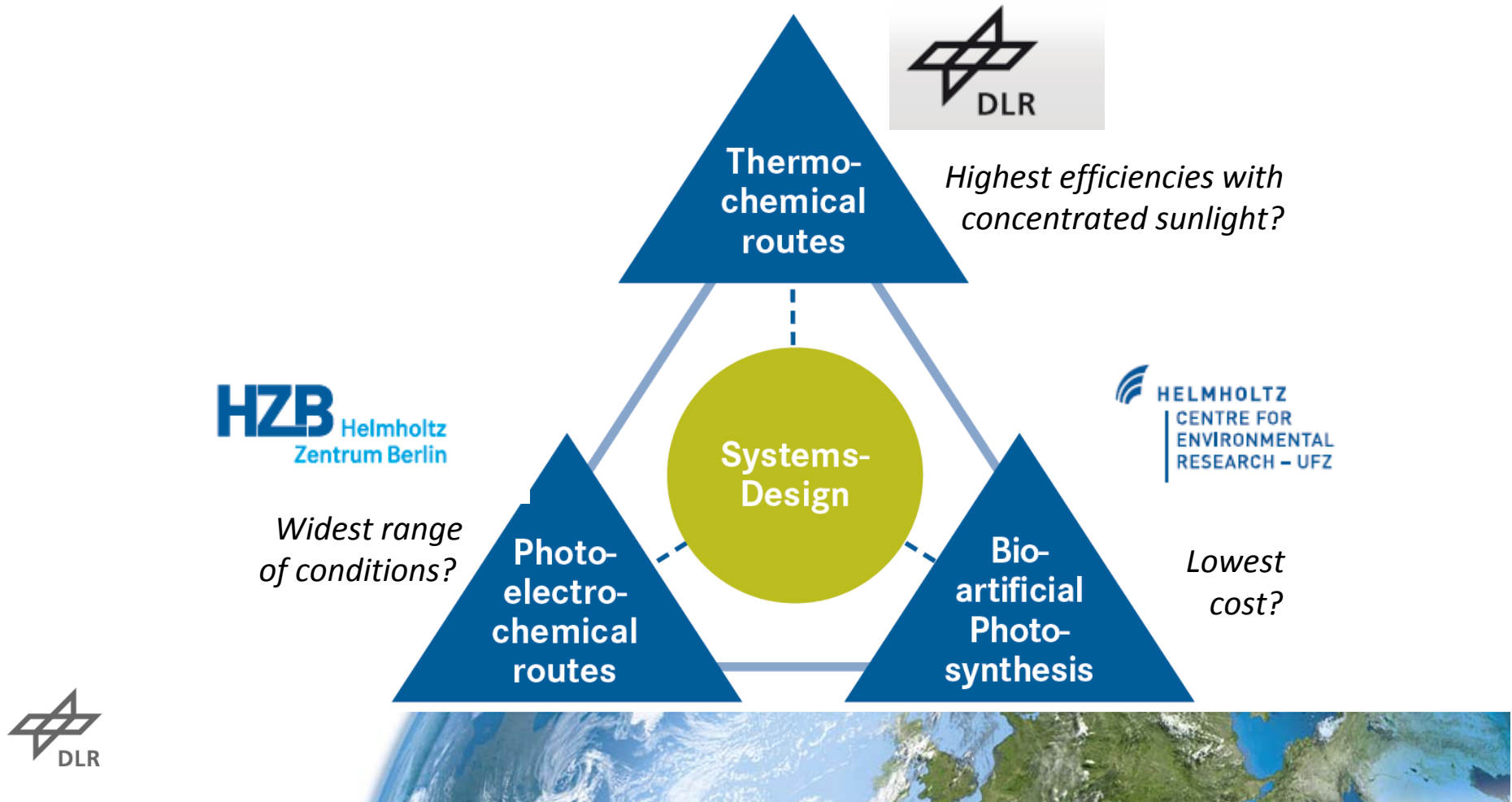
Solar Hydrogen



German Strategy and Approach on Solar Fuels

Goal in the Helmholtz Association

To demonstrate stand-alone, viable systems for the emission-free production of chemical fuels – especially **Hydrogen** - with sunlight



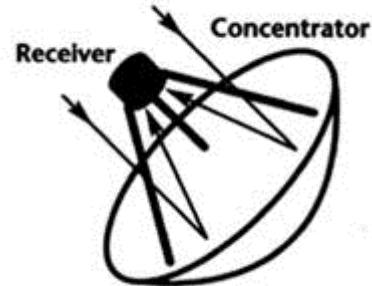
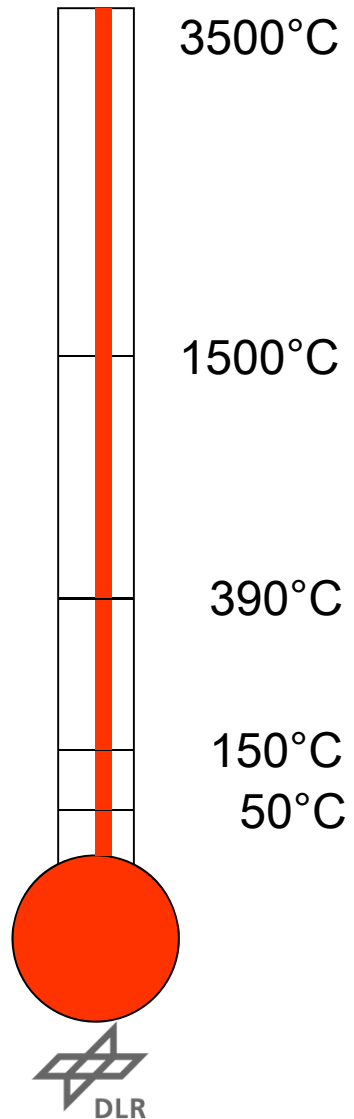
Efficiency comparison for solar hydrogen production from water (Siegel et al., 2013)*

Process	T [°C]	Solar plant	Solar- receiver + power [MW _{th}]	η T/C (HHV)	η Optical	η Receiver	η Annual Efficiency Solar – H ₂
Electrolysis (+solar-thermal power)	NA	Actual Solar tower	Molten Salt 700	30%	57%	83%	13%
High temperature steam electrolysis	850	Future Solar tower	Particle 700	45%	57%	76,2%	20%
Hybrid Sulfur- process	850	Future Solar tower	Particle 700	50%	57%	76%	22%
Hybrid Copper Chlorine-process	600	Future Solar tower	Molten Salt 700	44%	57%	83%	21%
Metaloxide two step Cycle	1800	Future Solar dish	Particle Reactor < 1	52%	77%	62%	25%

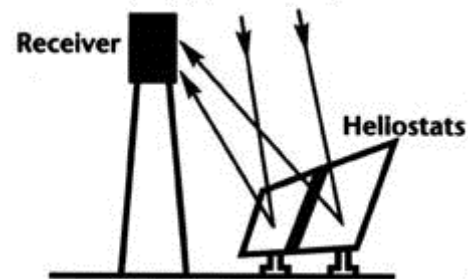
*N.P. Siegel, J.E. Miller, I. Ermanoski, R.B. Diver, E.B. Stechel, *Ind. Eng.Chem. Res.*, 2013, 52, 3276-3286.



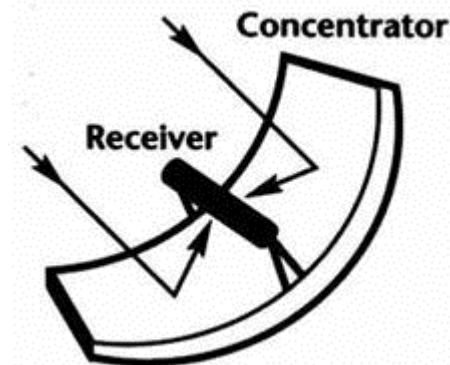
Temperature Levels of CSP Technologies



Paraboloid:
„Dish“



Solar Tower
(Central Receiver
System)



Parabolic Trough /
Linear Fresnel



Solar Towers



- PS10, Ivanpah, Torresol
- PSA CRS, CESA-1,
- Solar-Two, Daggett,



<http://www.ivanpahsolar.com/>



Solar Chemistry Research around the world

- Strong collaboration under the IEA “Solar Power and Chemical Energy Systems” (SolarPACES) program
www.solarpaces.org
- New IEA-HIA Task 35 on renewable hydrogen production



25 kW_{th} off-axis solar furnace
at DLR, Cologne (D)



20 kW_{th} HFSS at DLR, Cologne (D)



50 kW_{th} HFSS at PSI, Villigen (CH)



40 kW_{th} on-axis solar furnace
at PSI, Villigen (CH)



40 kW_{th} on-axis solar furnace
at KIER, Daejeon (KOR)



25 kW_{th} off-axis solar furnace
at NREL, Golden, CO (USA)



16 kW_{th} on-axis solar furnace
at Sandia, Albuquerque, NM (USA)



500 kW_{th} solar tower
at CSIRO, Newcastle (AUS)



1 MW_{th} solar furnace
at Parkent (Uzbekistan)



3 MW_{th} solar tower with “beam down”
optics at WIS, Rehovot (IL)

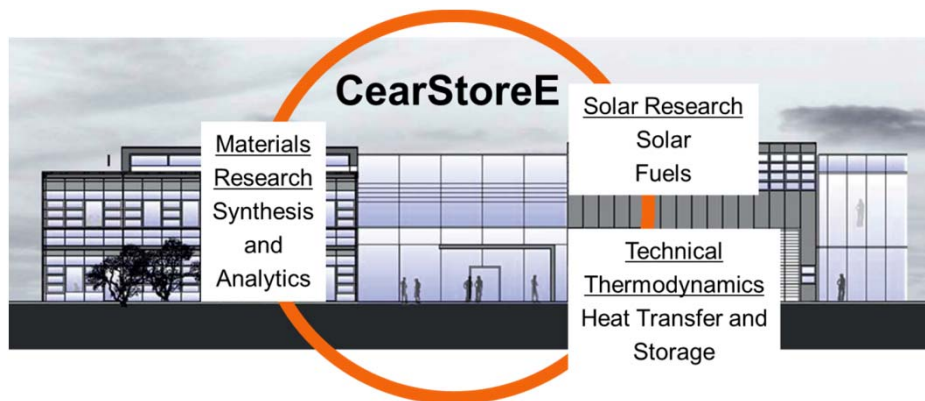


60 kW_{th} on-axis solar furnace
at Plataforma Solar de Almería (E)



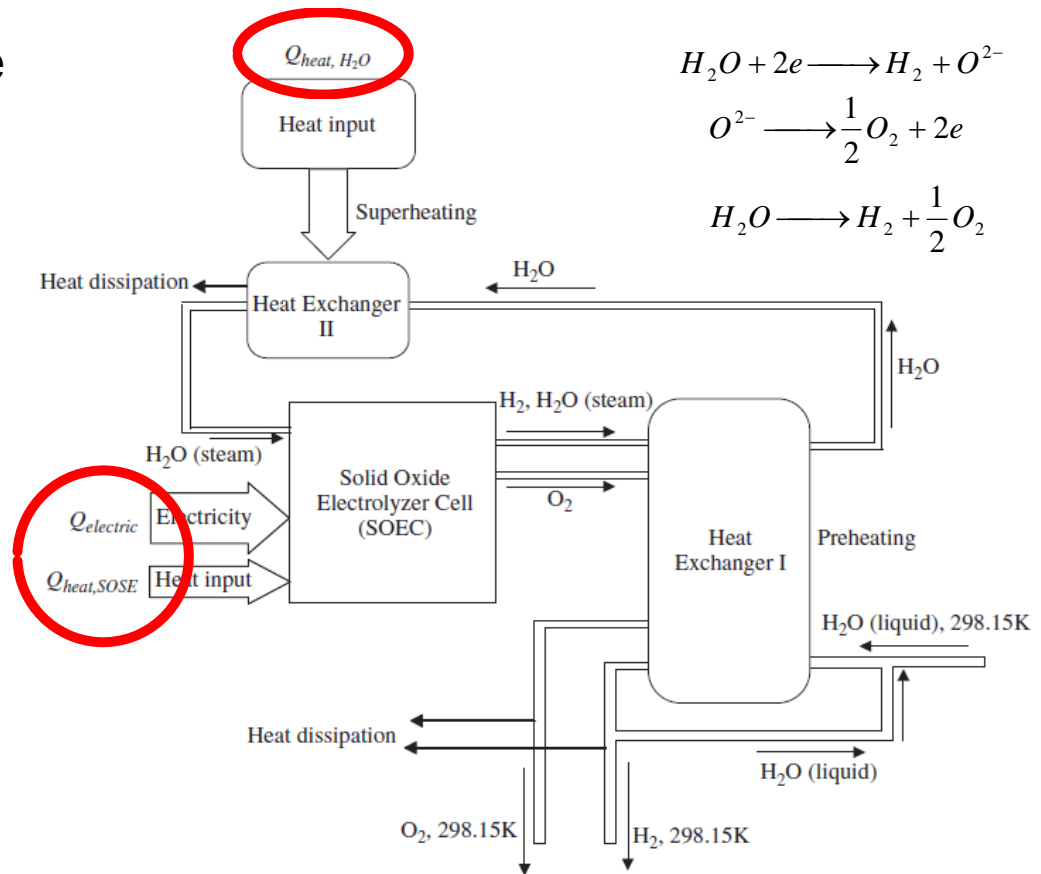
1 MW_{th} solar furnace
at CNRS-PROMES, Odeillo (F)

Large scale facilities used by DLR

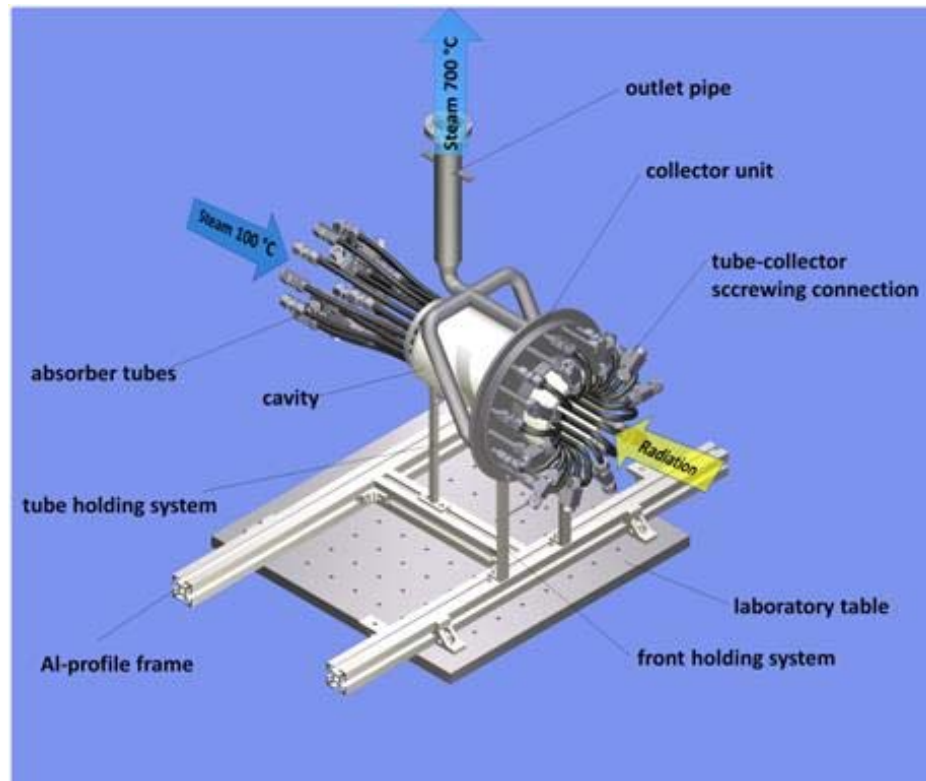


High temperature electrolysis process

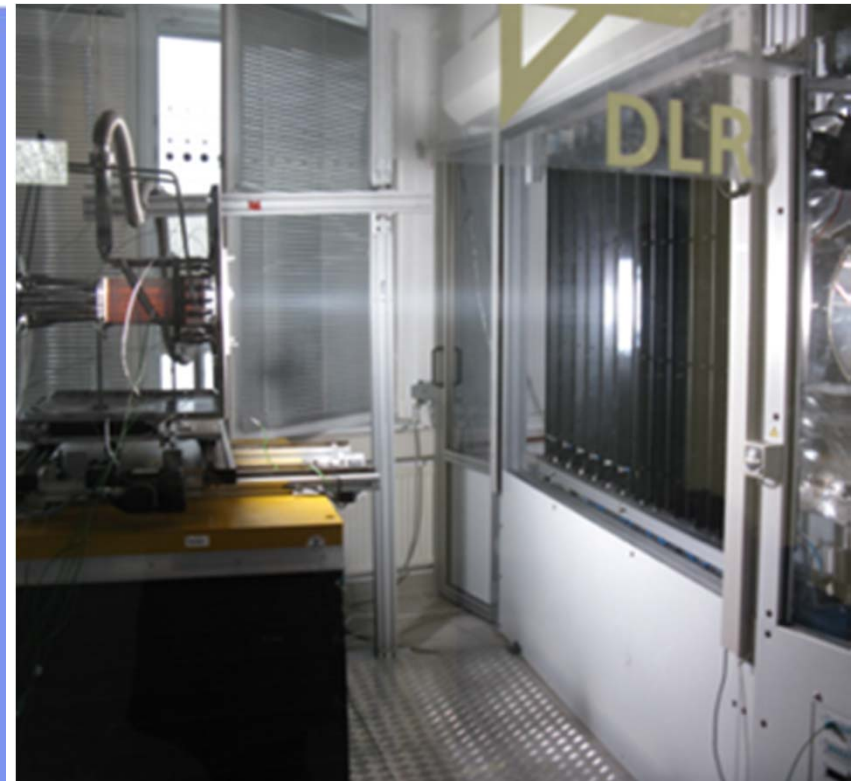
- Temperature in the range of 600°C to 900°C are required to drive the electrolyser.
- Electricity and heat are supplied to the electrolyser to drive the electro-chemicals reactions.
- The waste heat from the H₂ and O₂ gas streams existing the cell is used to evaporate water.
- The H₂O stream is further heated by the second Heat exchanger to raise the temperature of the electrolyser.



Solar Superheated Steam Generator for SOEC



3D Design

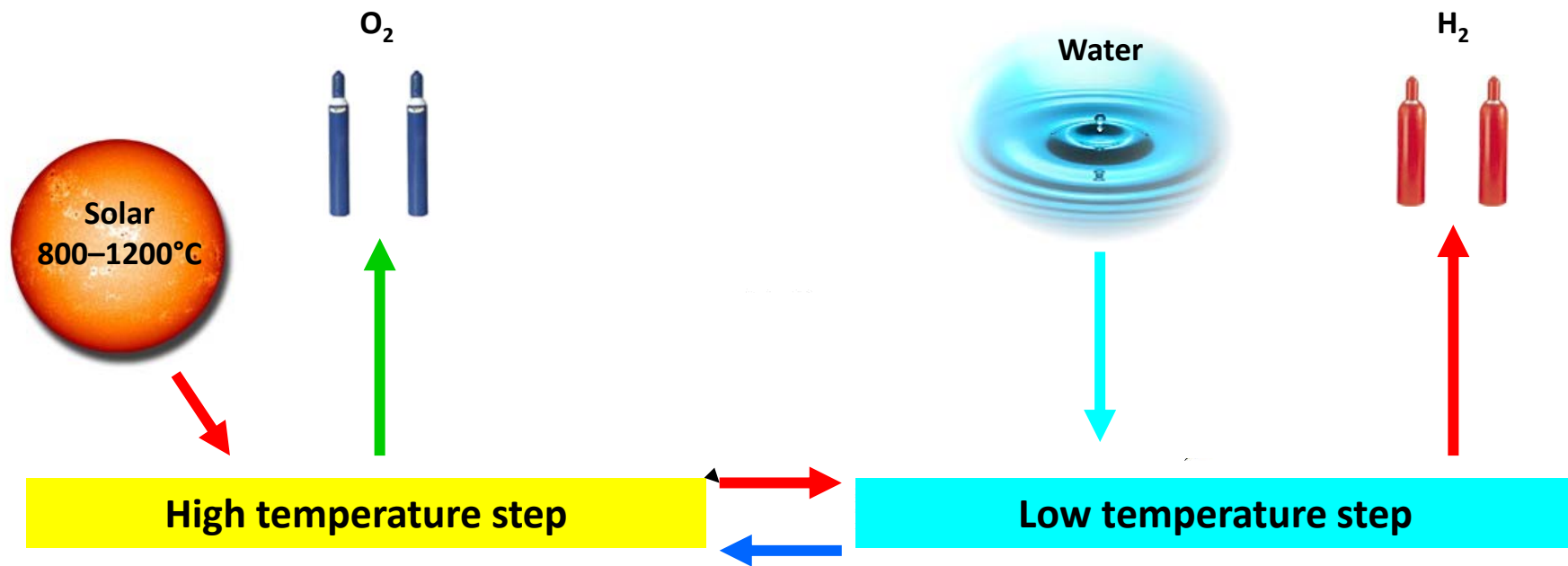


Operation in the solar simulator
providing 5 kg/h steam at 700 °C



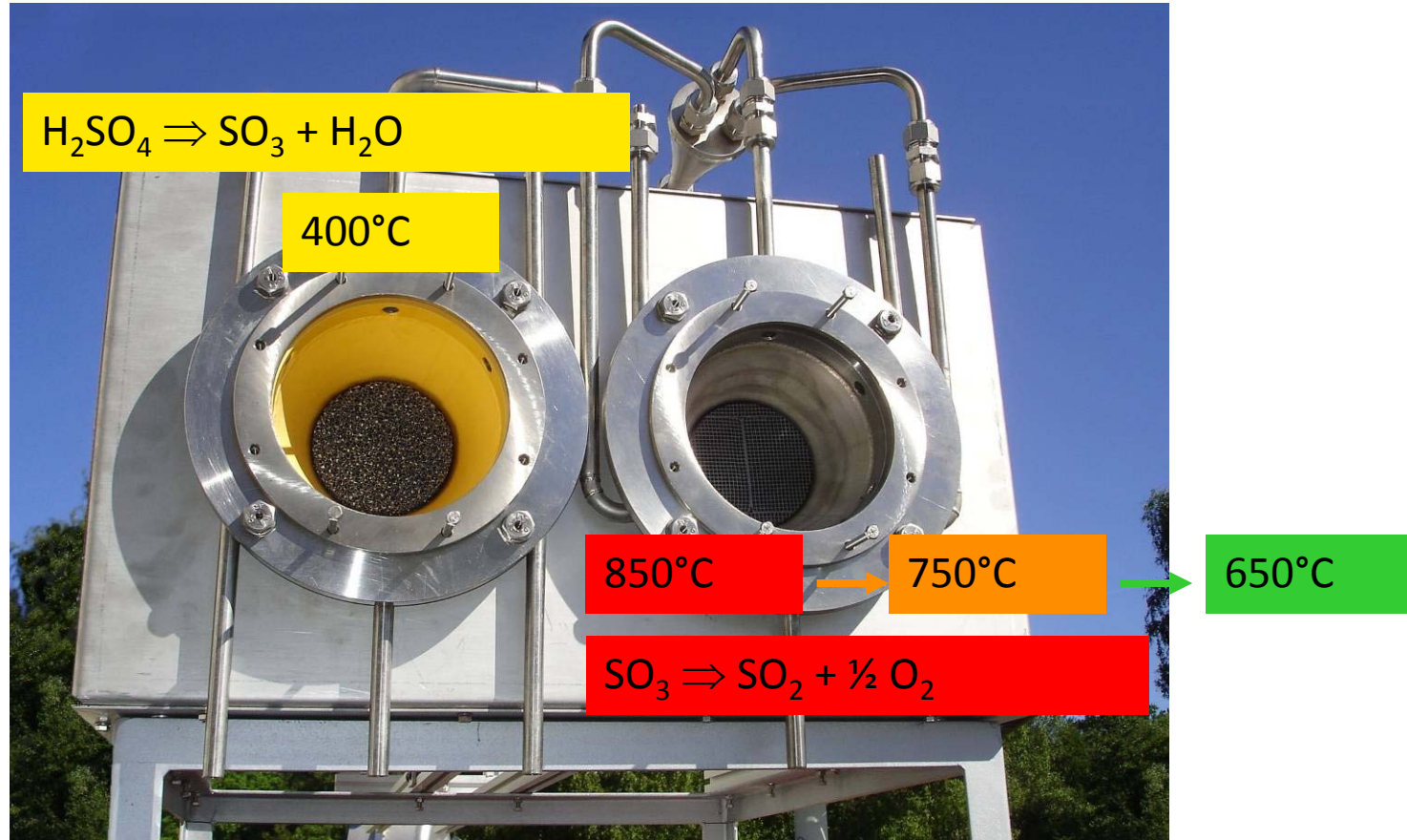


Hybrid Sulfur Cycle (HyS, Westinghouse)



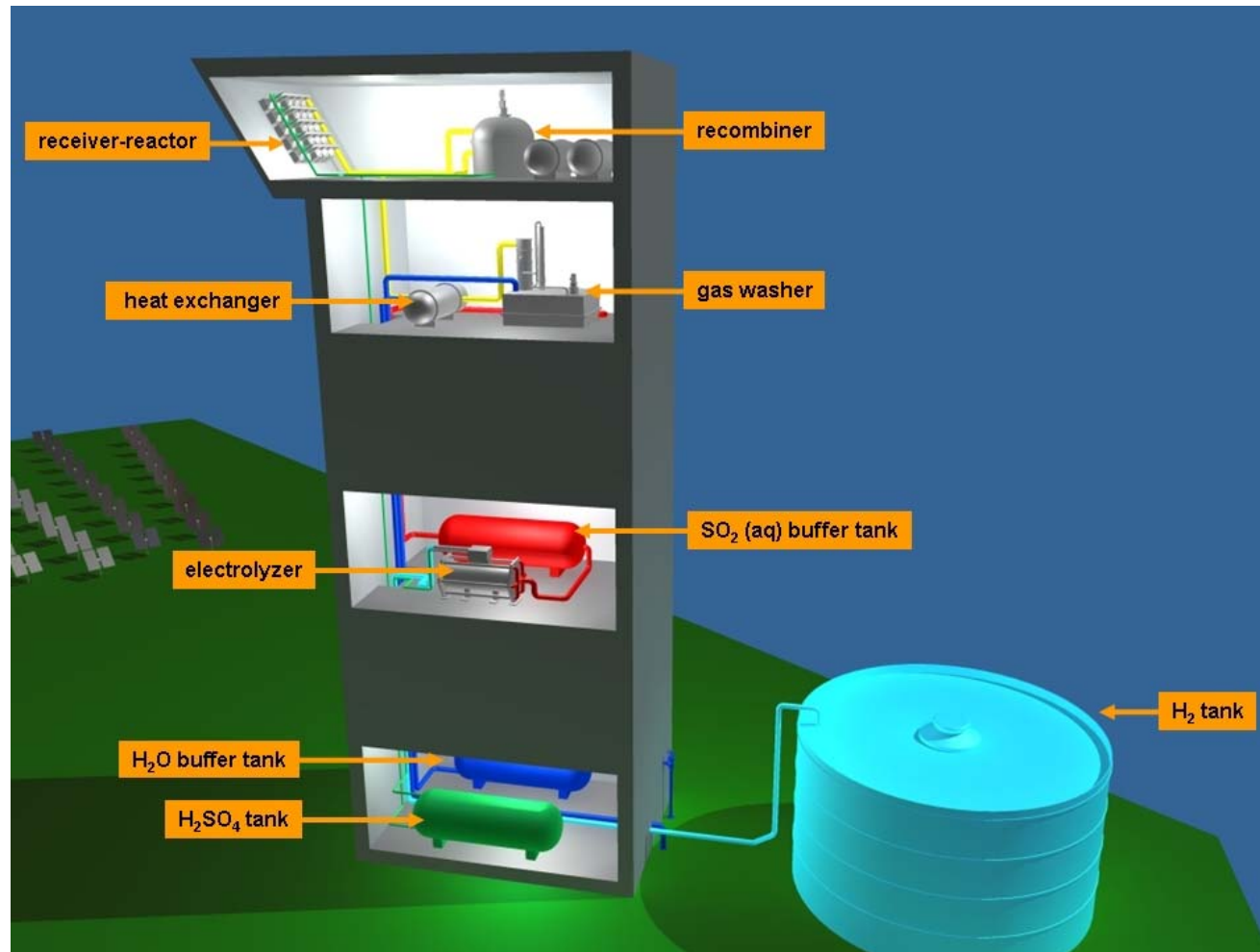


Solar reactor for sulfuric acid decomposition





Implementation into a Solar Tower





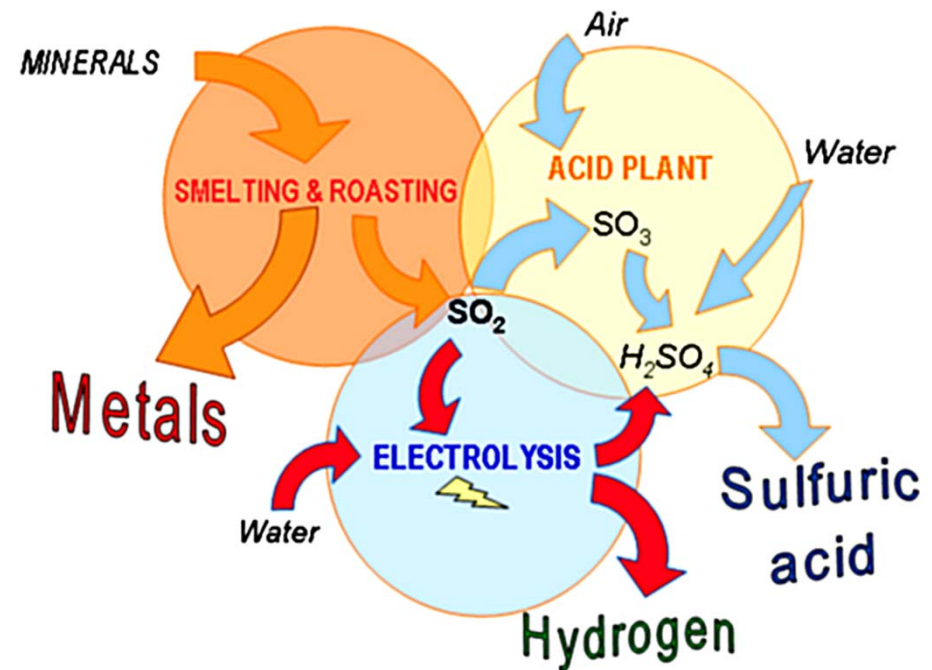
SOL2HY2 – Solar To Hydrogen Hybrid Cycles

- FCH JU project on the solar driven Utilization of waste SO_2 from fossil sources for co-production of hydrogen and sulphuric acid
- Hybridization by usage of renewable energy for electrolysis
- Partners: EngineSoft (IT), Aalto University (FI), DLR (DE), ENEA (IT), Outotec (FI), Erbicor (CH), Oy Voikoski (FI)
- >100 kW demonstration plant on the solar tower in Jülich, Germany in 2015

<https://sol2hy2.eurocoord.com>



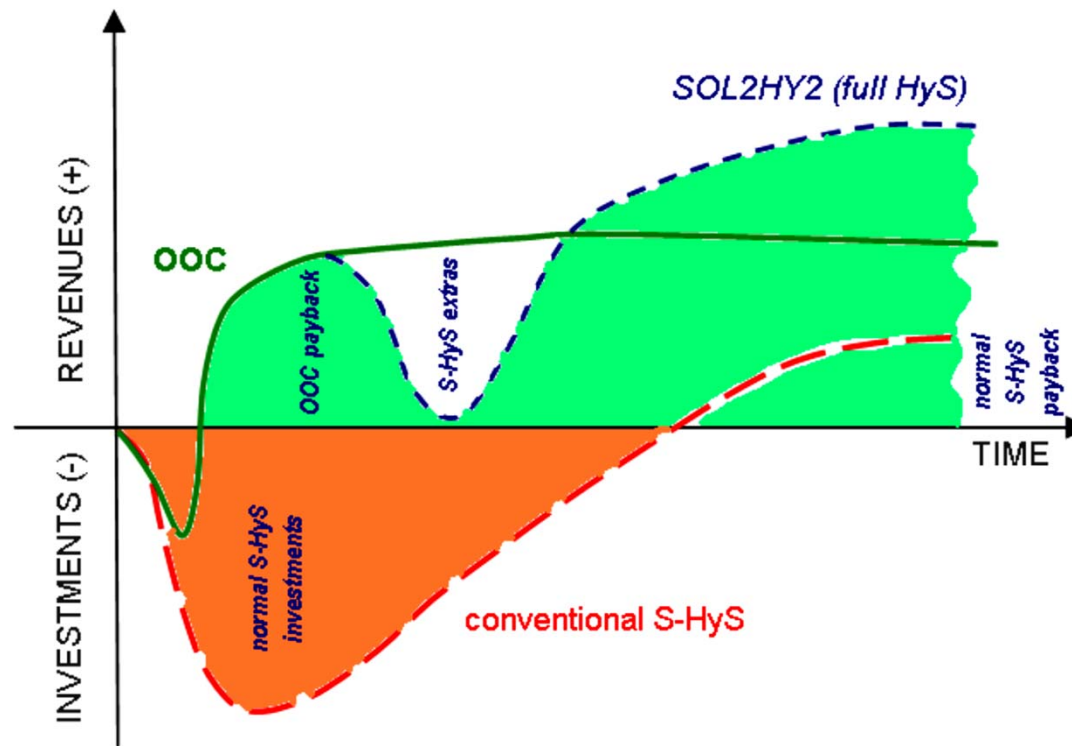
Outotec™ Open Cycle (OOC)



- Utilization of waste SO_2 from fossil sources
- Co-production of hydrogen and sulphuric acid
- Hybridization by renewable energy for electrolysis



Investments vs. revenues



- Reduction of initial investments
- Financing of HyS development by payback of OOC
- Increase of total revenues

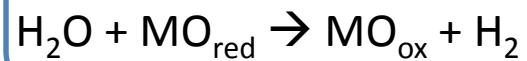




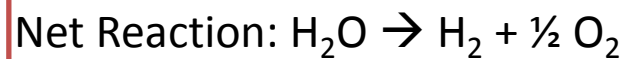
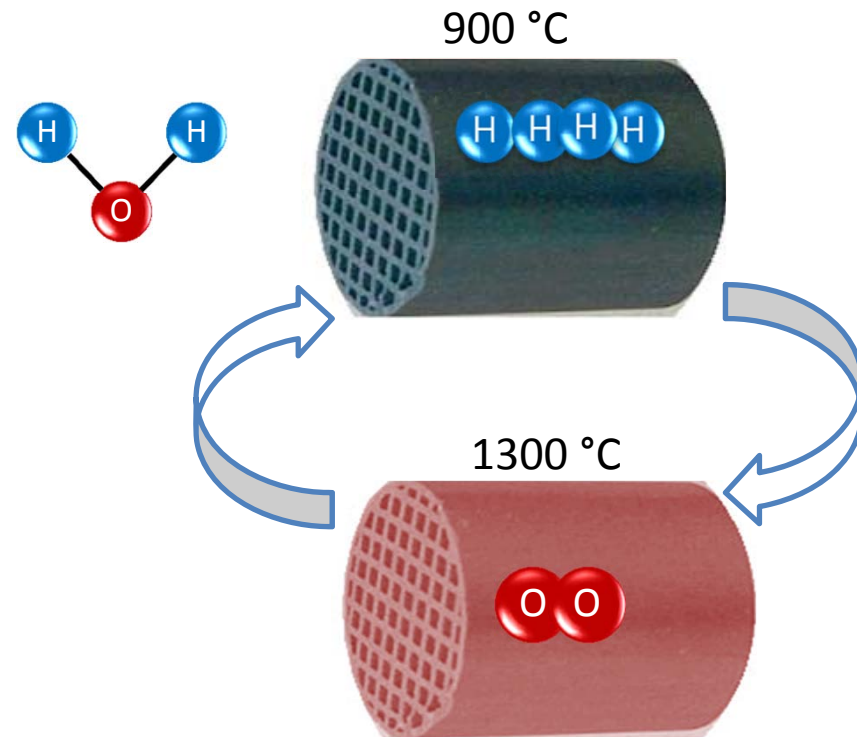
Example how a technology is developed

The HYDROSOL concept

1. Water Splitting



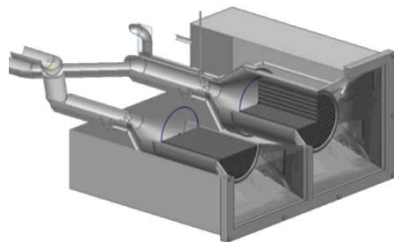
2. Regeneration





HYDROSOL Development

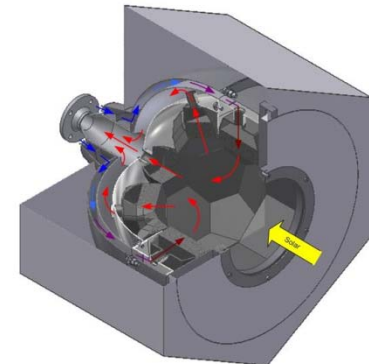
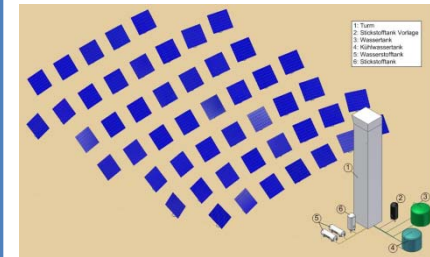
Hydrosol I
2002 – 2005
< 10 kW



Hydrosol II
2006 – 2009
100 kW



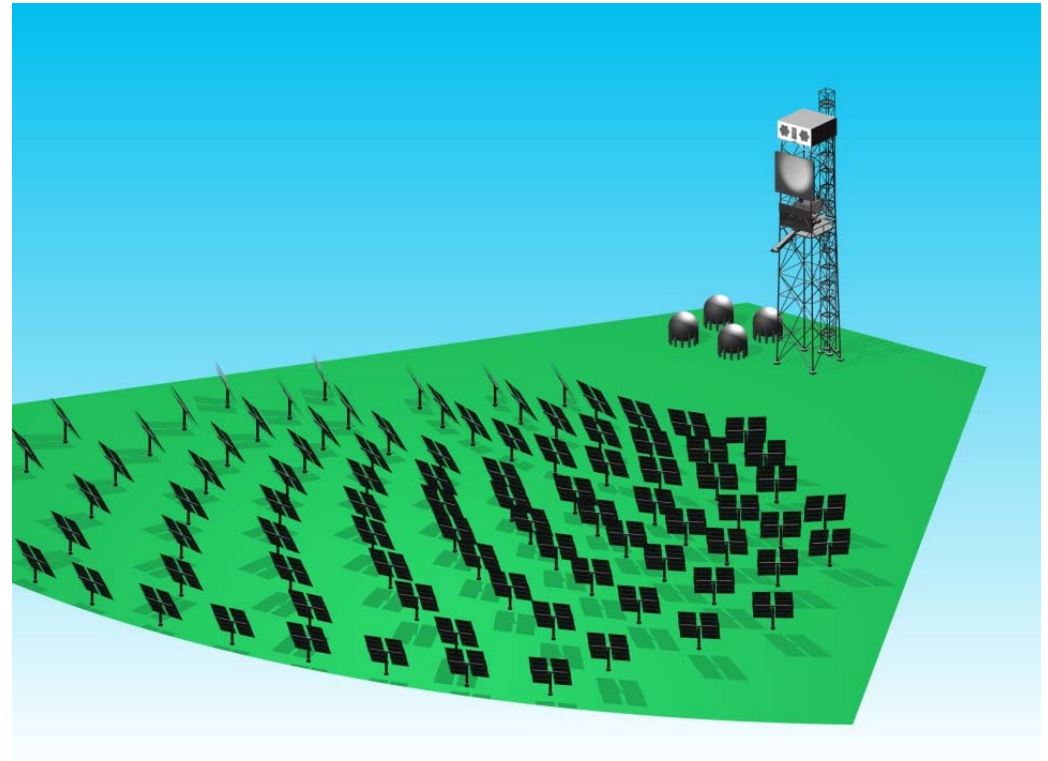
Hydrosol 3D
2010 – 2012
1 MW





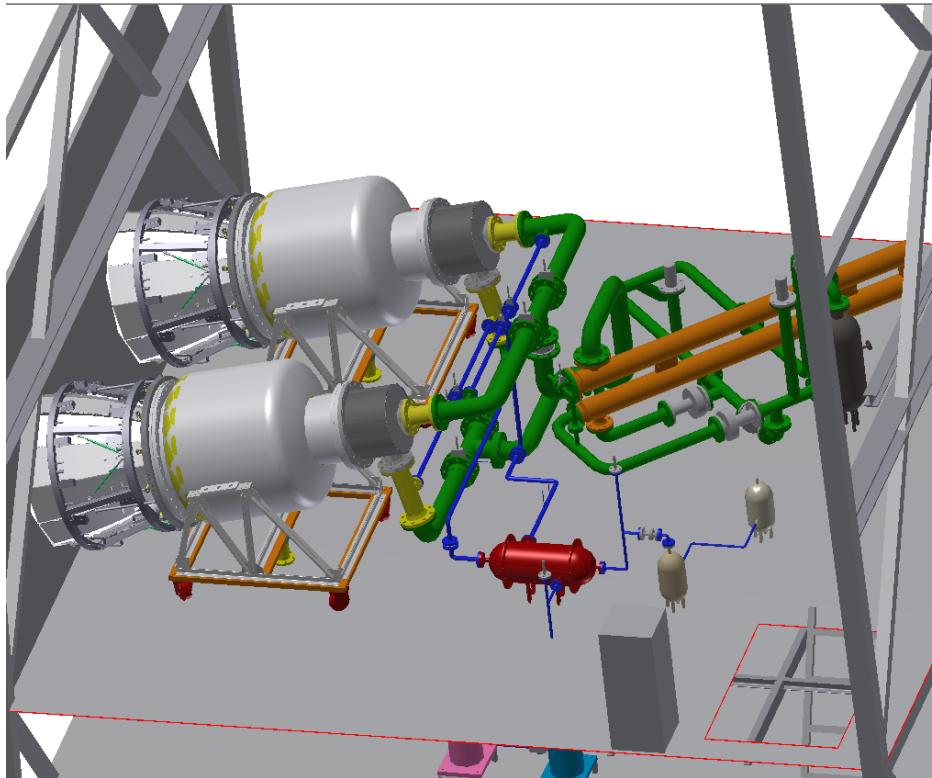
Hydrosol Plant - Design for CRS tower PSA, Spain

- European FCH-JU project
- Partner: APTL (GR), HELPE (GR), CIEMAT (ES), HYGear (NL)
- 750 kW_{th} demonstration of thermochemical water splitting
- Location: Plataforma Solar de Almería, Spain, 2016
- Use of all heliostats
- Reactor set-up on the CRS tower
- Storage tanks and PSA on the ground





HYDROSOL, HYDROSOL 2, HYDROSOL-3D, HYDROSOL Plant



APTL (GR), DLR (DE), CIEMAT (SP), StobbeTech (DK), Johnson Matthey (UK), HyGear (NL), HELPE (GR)



- **2002** Start HYDROSOL, EU FP5
- 2004 First solar hydrogen, DLR
- 2005 Quasi-continuous solar hydrogen, DLR
- 2008 HYDROSOL 2, EU FP6, 100 kW demonstration CRS Tower PSA, Spain
- 2013 HYDROSOL-3D, FCH JU, Design of a 1,5 MW demonstration plant ready
- 2014 HYDROSOL PLANT, FCH JU
- **2016** Operation of the 750 kW Demonstration plant, CRS Tower, PSA, Spain

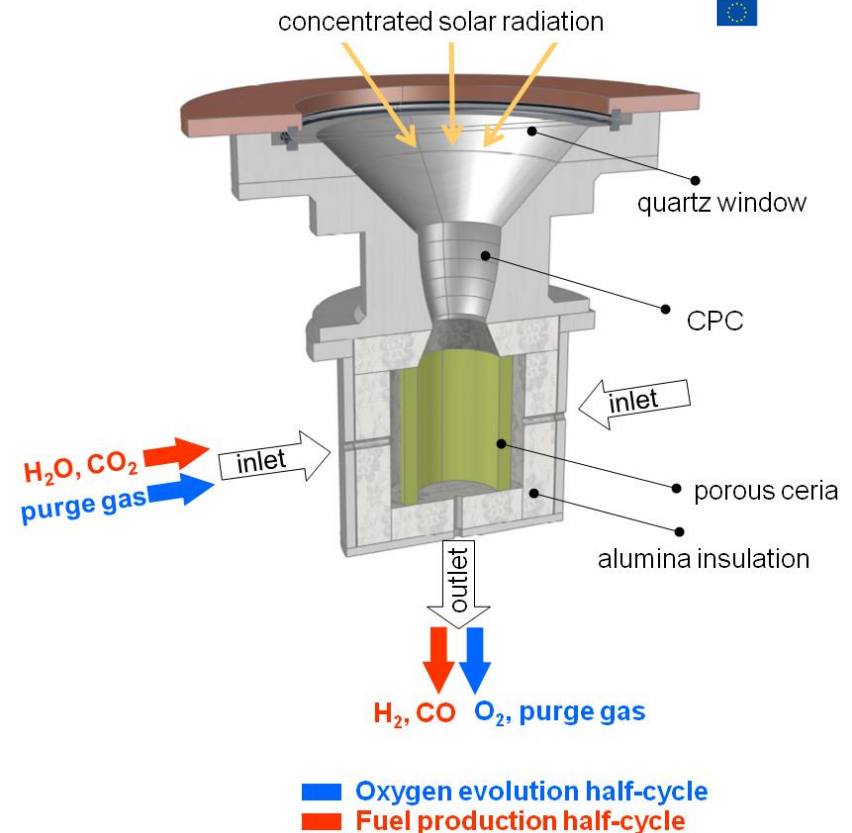
<http://hydrosol-plant.certh.gr/>



H₂O/CO₂-Splitting Thermochemical Cycles

Solar Production of Jet Fuel

- EU-FP7 Project SOLAR-JET (2011-2015)
- SOLAR-JET aims to ascertain the potential for producing jet fuel from concentrated sunlight, CO₂, and water.
- SOLAR-JET: optimize a two-step ceria based solar thermochemical cycle to produce synthesis gas (syngas) from CO₂ and water, achieving higher solar-to-fuel energy conversion efficiency over current bio and solar fuel processes.
- **First jet fuel produced in Fischer-Tropsch (FT) unit from solar-produced syngas!**



Int. J. Heat & Fluid Flow 29, 315-326, 2008.
Materials 5, 192-209, 2012.

Partners: Bauhaus Luftfahrt (D), ETH (CH),
DLR (D), SHELL (NL), ARTTIC (F)
Funding: EC

<http://www.solar-jet.aero/>

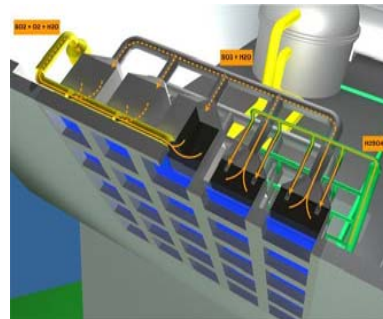


Technical Optimization in all Dimensions necessary



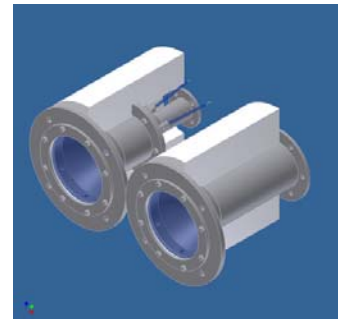
$10^4 - 10^2$ m
Solar Plant

Site
Solar field
Simulation
Environmental impact



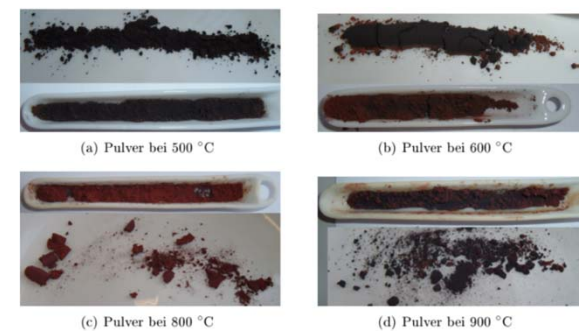
$10^2 - 10^1$ m
Receiver

Design
Simulation
Construction
Testing
Next-Generation-
Development



$10^1 - 10^{-2}$ m
Receiver-
components

Materials
Design
Heat and
Mass transport
Simulation
Testing and Development



$10^{-2} - 10^{-8}$ m
Reactive Systems

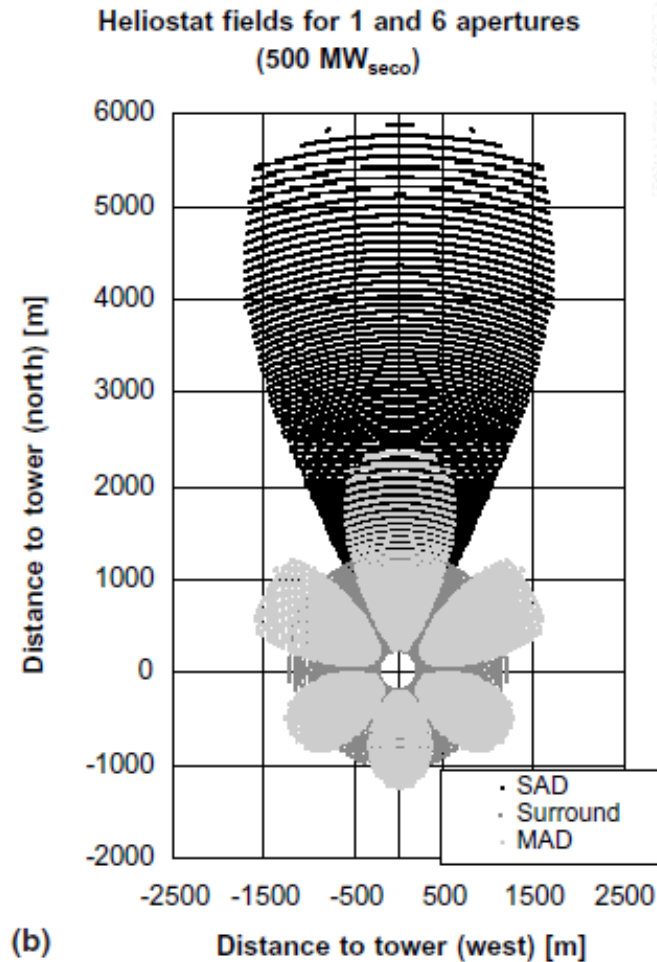
Simulation
Synthesis
Chemical Characteristics
Physical Characteristics



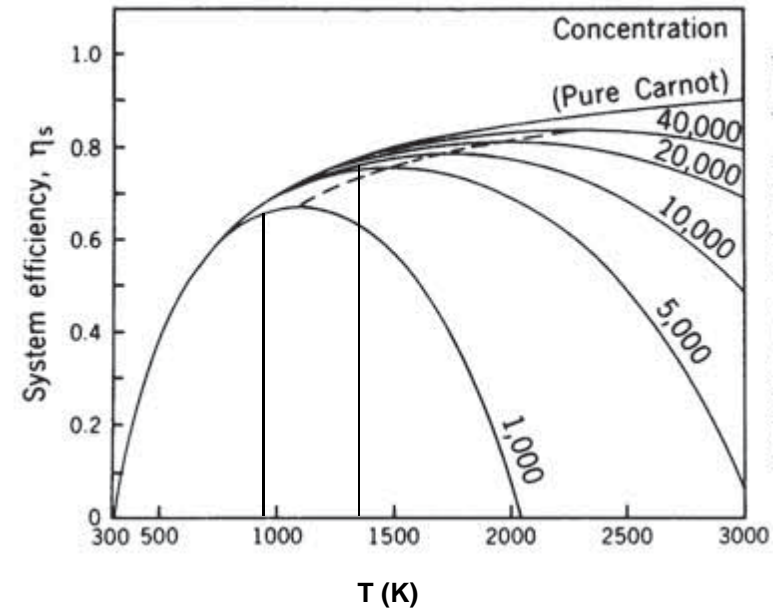
Solar Field Development

The field has to be designed for its application:

- Location
- Concentration ratio to achieve the Process temperature
- At high concentration (1000 suns) secondary optics have to be taken into account



M. Schmitz et al., Solar Energy 80 (2006) 111–120.

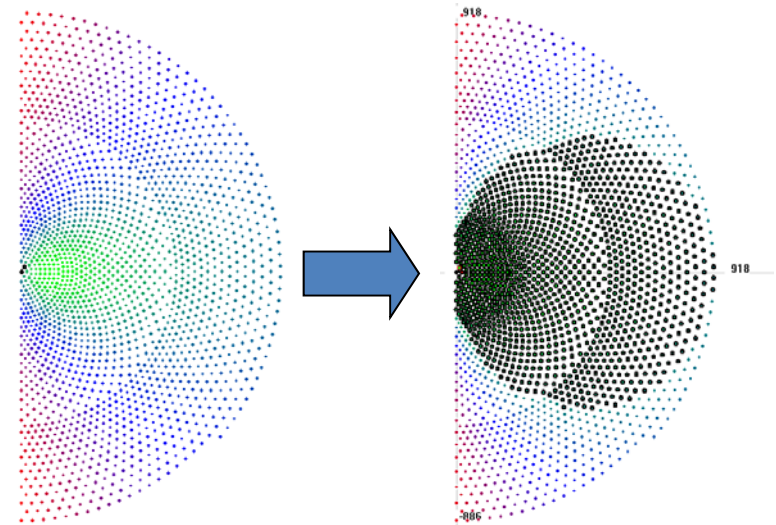


E.A. Fletcher, R.L. Moen, Science, 197 (1977) 1050-1056.

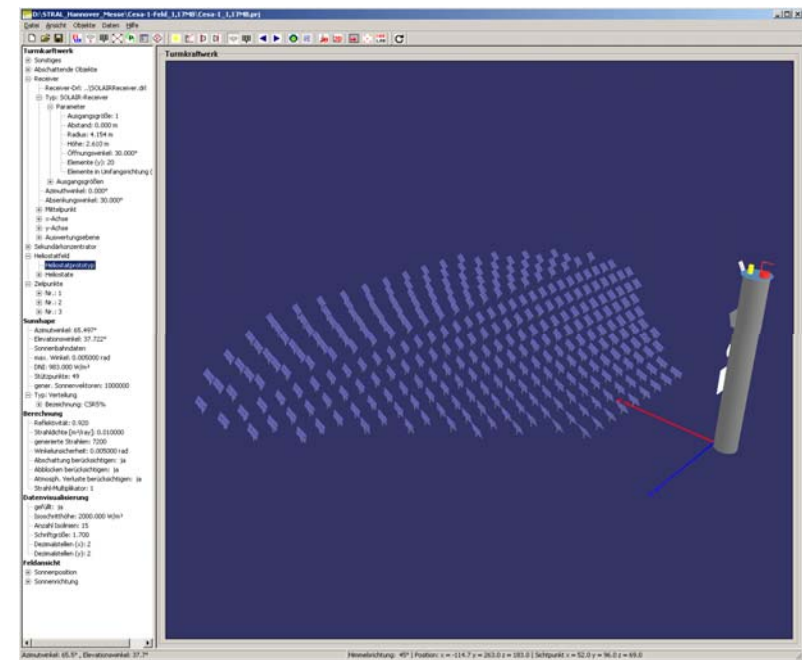


Simulation Tool Development for Solar Tower Systems

- Heliostat field layout

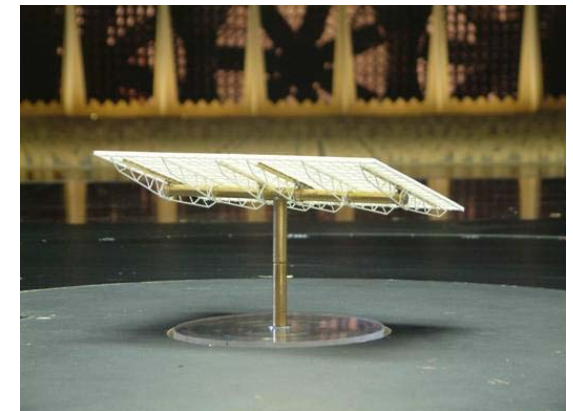
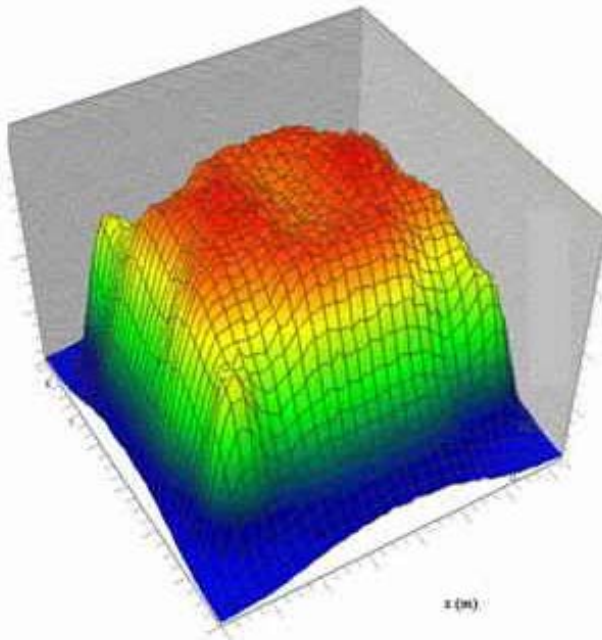
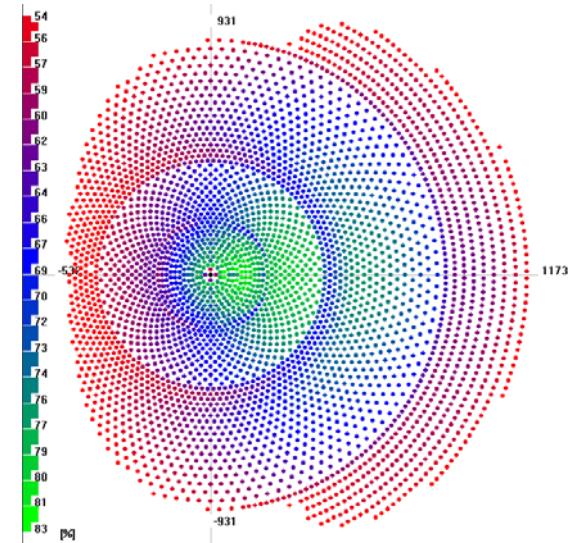
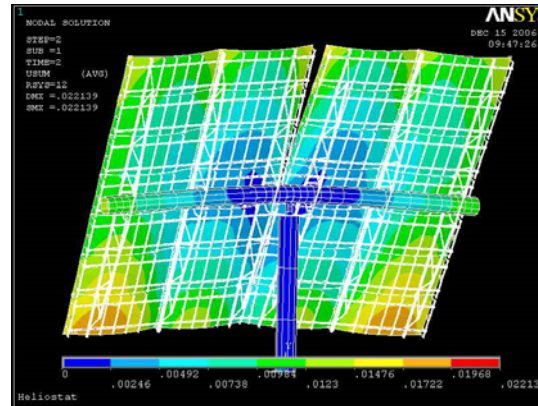


- Performance simulation
 - flux distribution
 - aim point strategy
 - efficiency



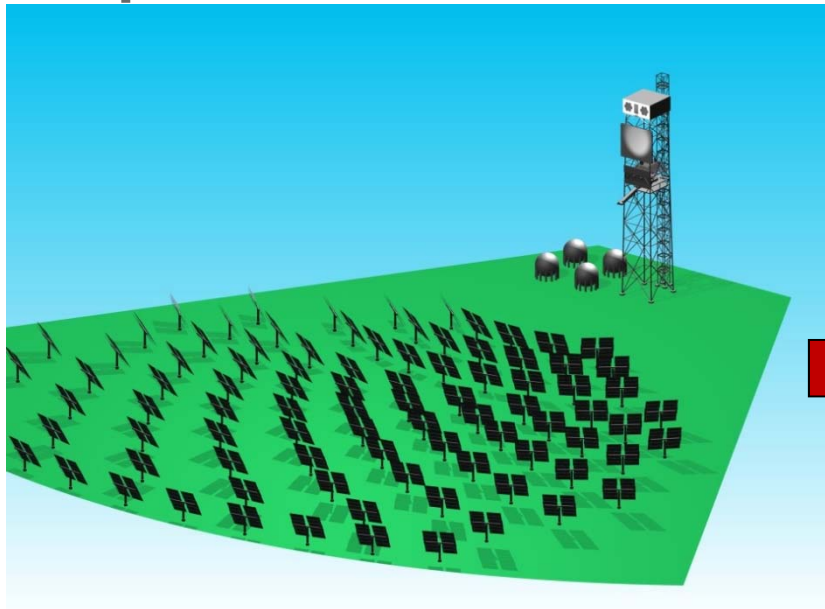
Heliostat R&D

- Heliostat and field simulation
- Structural analysis
- Load analysis
- Qualification
- Control
- Operation strategy

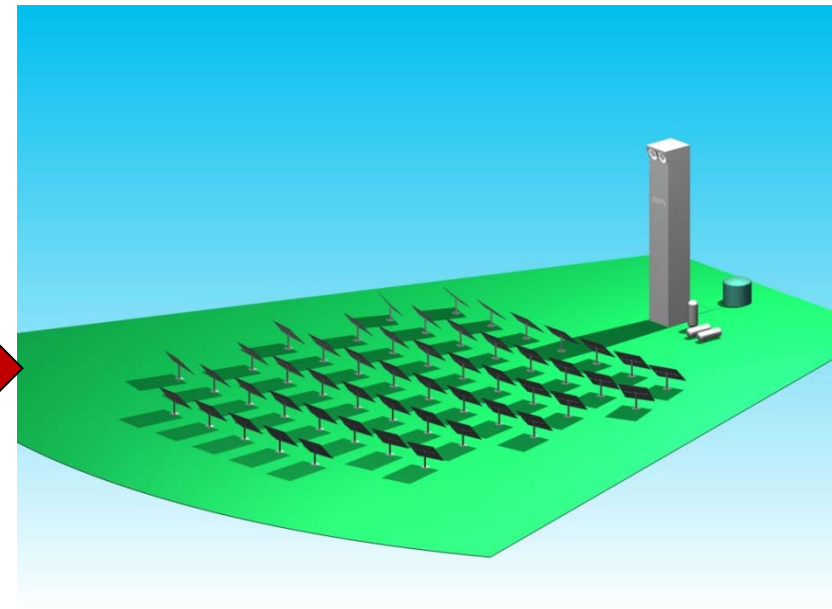




Next Step: Specific Solar Fuel Demonstration Tower needed!



CRS Tower PSA, Spain
2008 and 2016



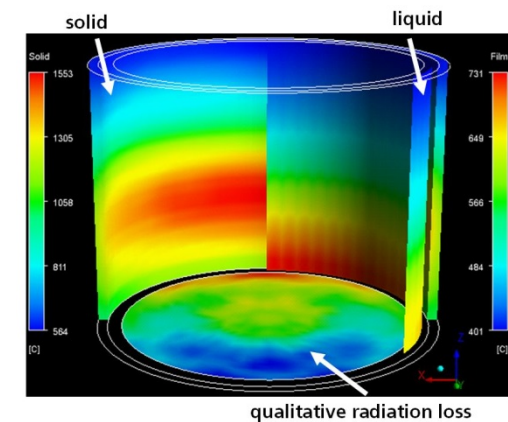
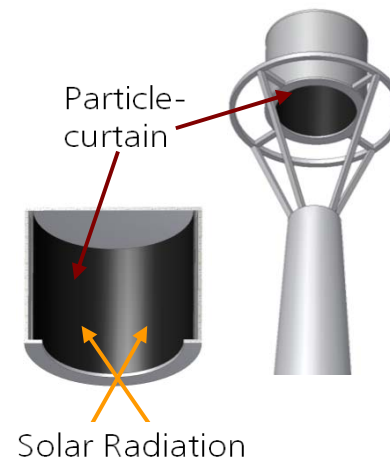
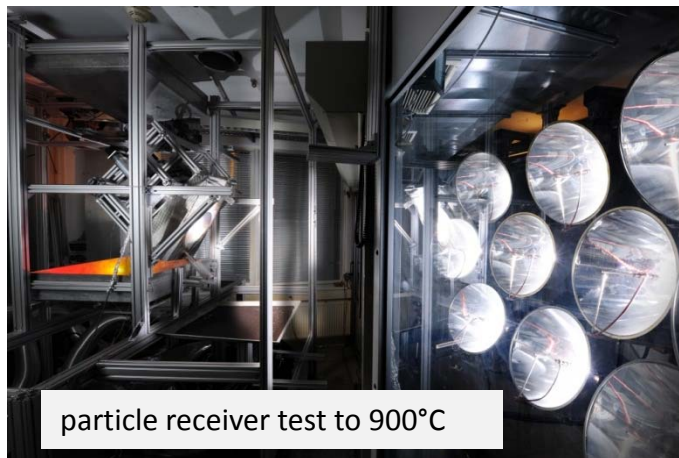
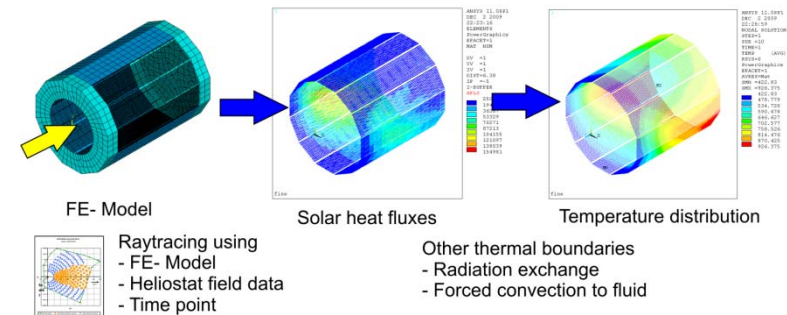
Solar Fuels Tower, Location?
2020

- High concentration > 1000
- Heliostats fit to receiver size
- Field control adapted to fuel production processes



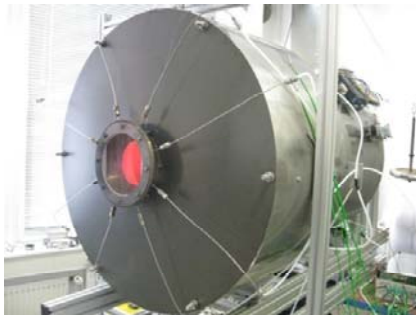
Receiver Technology R&D

- Development / technology transfer
 - open volumetric air receivers
 - pressurized air receivers
- Extension to liquid heat transfer media
 - e. g. molten salt
- Innovative concepts: direct absorption receivers

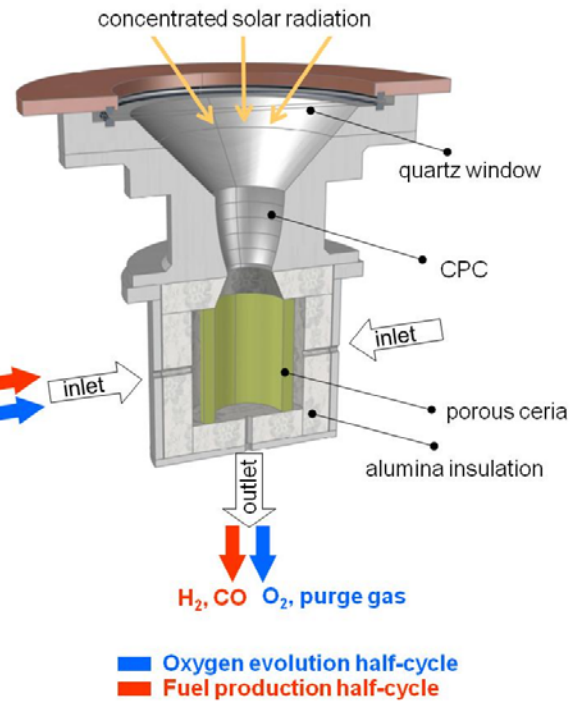
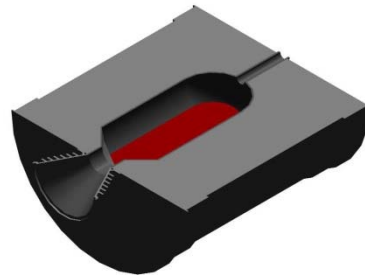


Receiver – Concepts for Solar Chemistry

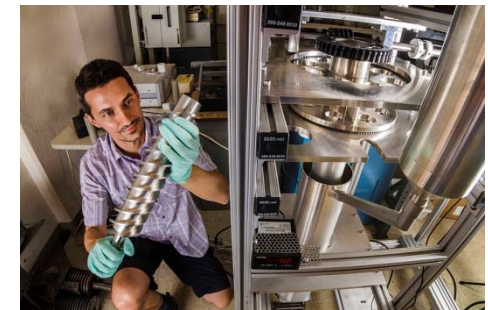
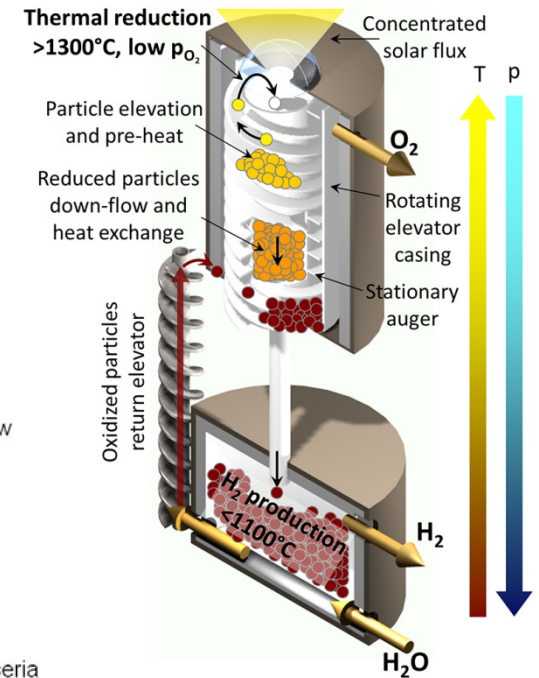
- Challenges:
 - Temperature
 - Corrosion
 - Abrasion
 - Process operation
- Goals:
 - Efficiency
 - Durability
 - Cost



German Project
Solar heated rotary kiln, DLR



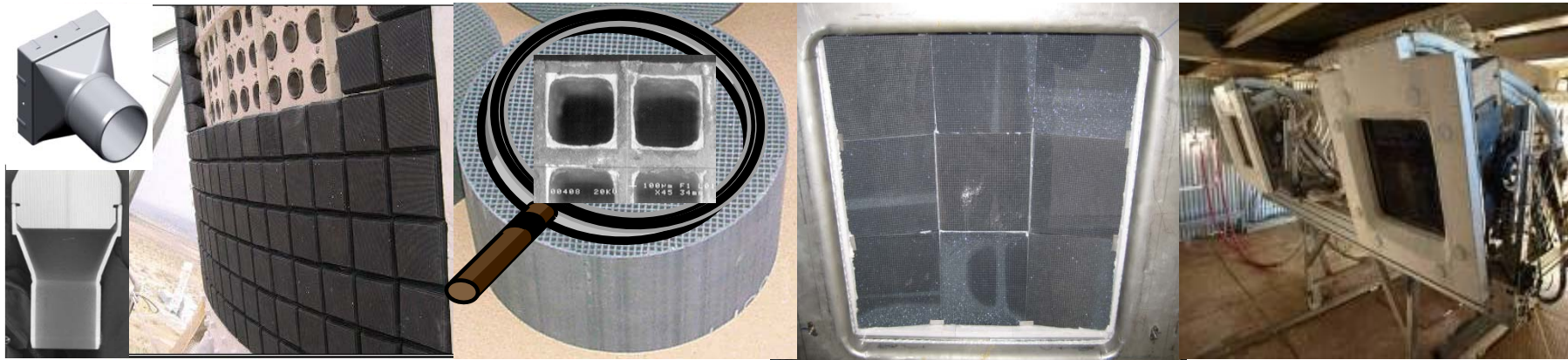
European Project
Solar heated Cavity-Gas Receiver
with porous Ceramic structur
A. Steinfeld et al., ETH Zürich



DoE Project with DLR participation
Solar heated Particle-Receiver
I. Ermanoski et al., Sandia Natl. Lab.



Solar Receiver Components and reactive Systems



C. Agrafiotis, M. Roeb, A.G. Konstandopoulos, L. Nalbandian, V.T. Zaspalis, C. Sattler, P. Stobbe, A.M. Steele, Solar water splitting for hydrogen production with monolithic reactor, *Solar Energy*, 79(4), 409-421, (2005).

Reactive coated structures and structures made from reactive materials



P. Furler, J. Scheffe, M.Gorbar, L. Moes, U. Vogt, A. Steinfeld, Solar Thermochemical CO₂ Splitting Utilizing a Reticulated Porous Ceria Redox System, *Energy & Fuels*, 26(11), 7051-59, (2012).



Overview of DLR CSP simulation tools

- DLR simulation tools cover all levels of CSP simulation

GREENIUS: analysis of performance / economics of renewable energy systems

ebsSolar®: detailed performance analysis of CSP systems

component layout:

- concentrators (parabolic trough, Fresnel, heliostats)
- receivers

system layout optimization:

- solar field, receiver
- power block
- storage

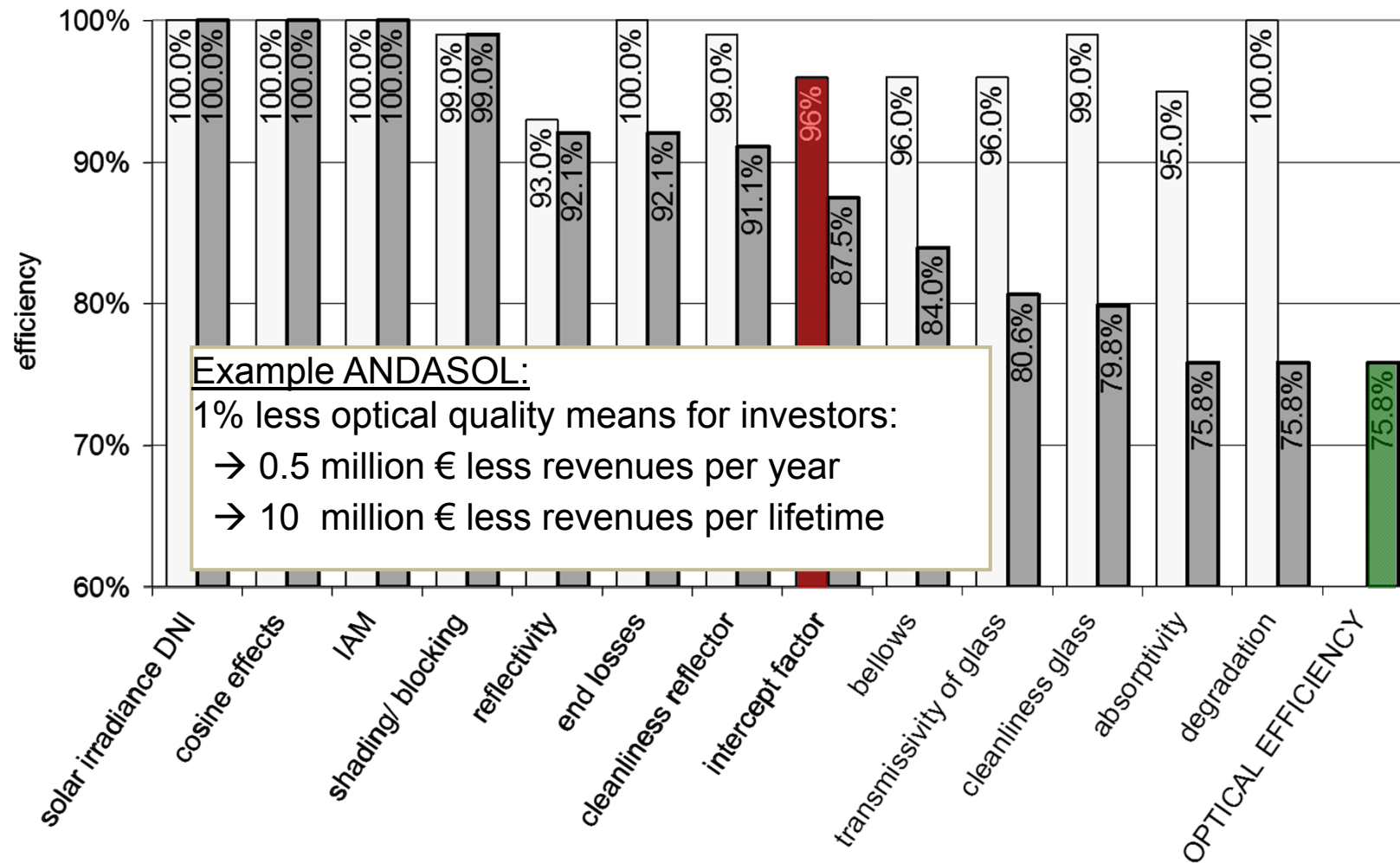
transient system simulation:

- real-time, high resolution performance simulation
- coupling of components and control



Qualification - Motivation

Efficiency Chain, Example: Parabolic Trough



QUARZ® – Center Test and Qualification Center for CSP Technologies

- Strong impact on the **performance and cost efficiency**:
 - CSP component quality and durability
 - their interaction in the overall system
 - and the meteorological conditions each
- Development of **measurement techniques and devices**
- Evolution of **guidelines and standards**
 - testing methods
 - quality criteria
- Customer oriented services
 - Fundamental information for industry to
 - **Improve** quality, performance → **competitiveness**
 - **Proof** of product quality → successful **market entry / bankability**
 - Consulting and training



EERA – European Energy Research Alliance



EERA supports the EU SET-Plan by accelerating the development of energy technologies through joint R&D



EERA reinforces Europe's role by supporting the competitiveness of industry at international level.

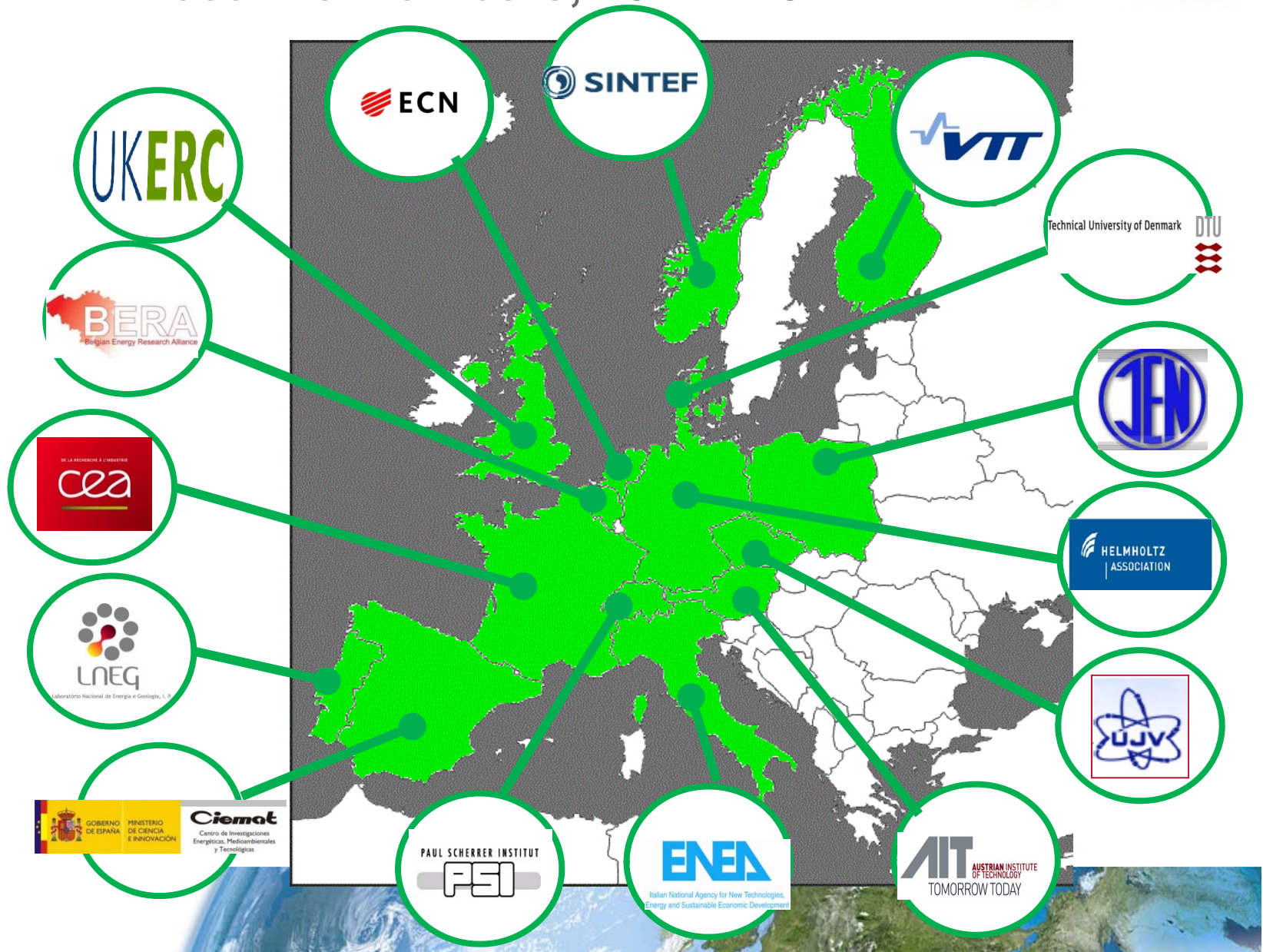


The relevance of research will be enhanced in close cooperation with Member States, the EC and industry to support the political and industrial SET-PLAN objectives.



EERA – Executive Members, 2012 - 2014

Supported
by :





EERA – Joint Programmes (JPs)

Joint Programmes launched 2010

- Bioenergy
- CCS
- Geothermal
- Mat. for Nuclear
- PV
- Smart Grids
- Wind

Overall 15 EERA
Joint Programmes



Joint Programmes launched 2013

- JP on socio economic impact
- Shale Gas

Joint Programmes launched 2011

- AMPEA (Materials & Processes)
- **CSP**
- Energy Storage
- **Full Cells & Hydrogen**
- Ocean Energy
- Smart Cities





FP7 – Integrated Research Programmes (IRP)

<u>Funding</u>	<u>Proposal</u>	<u>Topic</u>
Yes	STAGE-STE	CSP
Yes	ELECTRA	Smart <u>Grids</u>
Yes	IRPWIND	Wind
Yes	CHEETAH	PV
No	BIOENERGY IRP	<u>Bio-energy</u>
No	EESTORIGA	Energy Storage

EERA will:

- Coordinate common set of KPIs
 - Evaluate the different mobility schemes
 - Compare situation of national programmes
 - Identify common elements of IRP consortium agreements
 - ...
- for preparing future EERA IRPs or European Co-Fund Actions



STAGE-STE Consortium (today)

www.stage-ste.eu

Organisation name	Country
CIEMAT	SPAIN
DLR	GERMANY
PSI	SWITZERLAND
CNRS	FRANCE
FISE	GERMANY
ENEA	ITALY
ETHZ	SWITZERLAND
CEA	FRANCE
CYI	CYPRUS
LNEG	PORTUGAL
CTAER	SPAIN
CNR	ITALY
CENER	SPAIN
TECN	SPAIN
UEVORA	PORTUGAL
IMDEA	SPAIN
CRAN	UK
TKN	SPAIN
UNIPA	ITALY
CRS4	ITALY

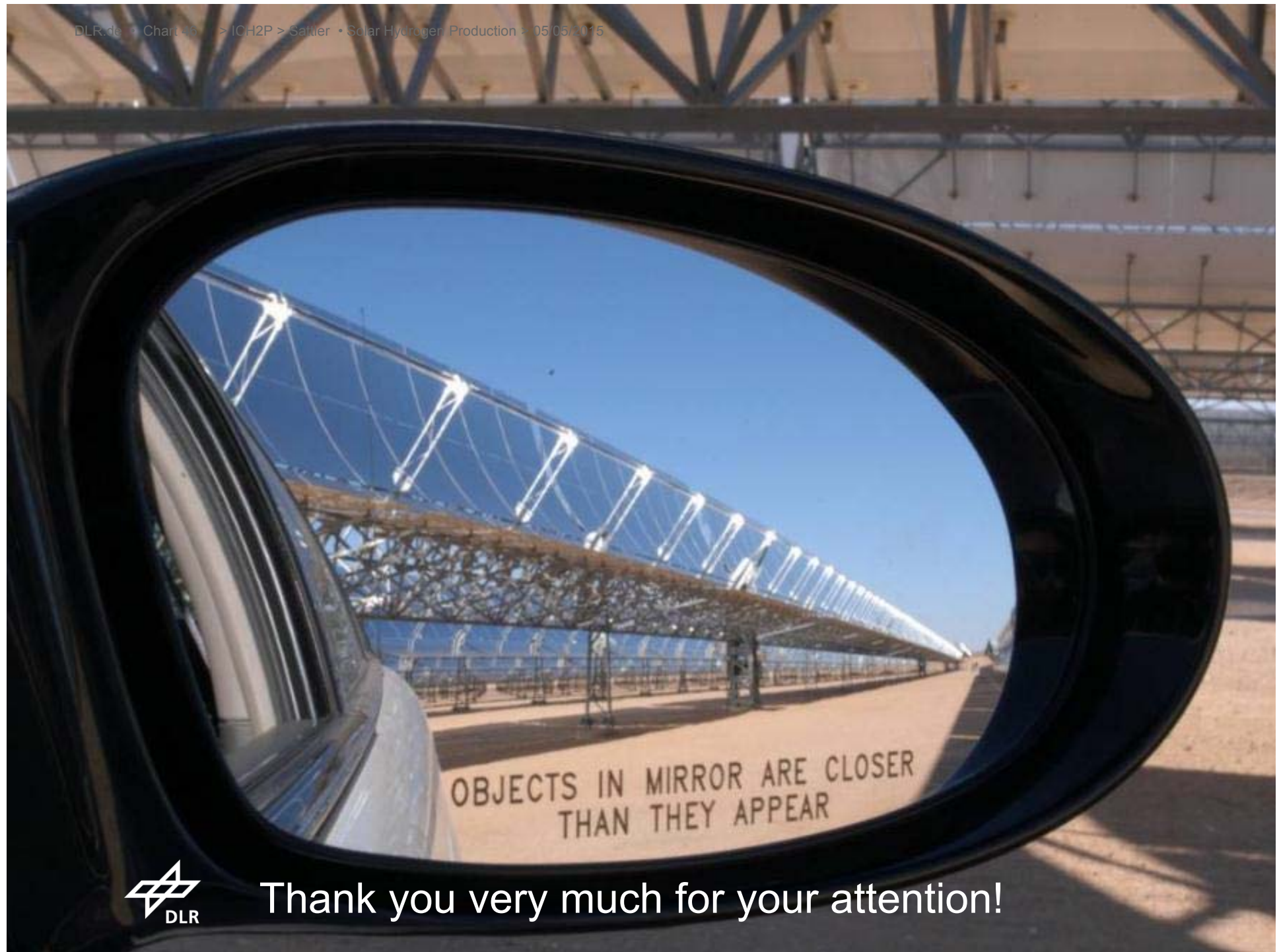
Organisation name	Country
INESC-ID	PORTUGAL
IST-ID	PORTUGAL
SENER	SPAIN
HITIT	TURKEY
ACCIONA	SPAIN
SCHOTT	GERMANY
ASE	ITALY
ESTELA	BELGIUM
ABENGOA Solar	SPAIN
ASNT	SPAIN
KSU	SAUDI ARABIA
UNAM	MEXICO
SUN	SOUTH AFRICA
CSERS	LYBIA
CSIRO	AUSTRALIA
FUSP	BRAZIL
IEECAS	CHINA
UDC	CHILE
UCAM	MOROCCO
FBK	ITALY



Summary and Outlook

- Hydrogen will play a **key role** in reducing CO₂ emissions
- **Synergies** between hydrogen production technologies should be used to
 - Accelerate **development and deployment**
 - Raise the **acceptance** for hydrogen in the society
 - **Support industry** to be successful with innovative technologies
- Solar thermochemical processes have a high potential to be efficient renewable pathways for **large scale hydrogen production**
- Technologies are **demonstrated** in the > 100 kW_{th} range
- Further **developments and demonstrations** are necessary to achieve a **market introduction**
- Acknowledgement: Thanks to everyone who contribute to the development of sustainable hydrogen production, especially the European Commission for funding projects within the FCH-JU and the RFPs





Thank you very much for your attention!